

Rapport final, 31 décembre 2006

Projet

Caractéristiques des pompes fonctionnant en turbines

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N° projet / n° contrat OFEN	101712 / 152106, suite de 100400 / 150 497
Durée prévue du projet (de - à)	08.10.2003 – 31.12.2006 (avenant: le 30.11.2004) pour 100400 01.06.2007 – 31.01.2007 (contrat 152106 du 01.06.2006) pour le 101712

ABSTRACT

Thanks to the partnership between OFEN, Sulzer, EIG and HEVS important improvements for the determination of performance of pumps as turbines and for the use of small variable speed generators in small power plants have been done.

The method proposed is based on the determination of a model which computes the total head losses in pump operation with the help of the pump geometry. Then, this model is applied to determine the characteristics in turbine operation.

The pump model has been divided in elements connected in series and in parallel from the inlet to the exit of the pump. The calculation of hydraulic losses in each element (friction losses, bend losses, gradual expansion and contraction, sudden expansion or contraction) has been performed and the sum of those gives the total head losses through the pump.

For this project, 5 pump geometries have been used in order to verify the model. One belongs to the EIG and measurements have been performed to determine the geometry and the pump and turbine characteristics. The other 4 geometries and their characteristics have been provided by Sulzer Pumps.

As results, the model of losses allows a prediction of the head at the best efficiency point (BEP) in pump operation with a shift between 4 and 5 %.

In turbine operation, by comparing the turbine characteristics predicted and the experimental data, a shift from 2 to 5% is observed at the BEP.

A software programmed in Excel has been developed and it will be available for free use.

At the HEVS, a laboratory test rig has been built and is composed of a permanent magnet synchronous generator as well as a frequency converter developed at this institution. The test rig allows testing the control algorithms. The results show a good efficiency at part load operation. A paper concerning this generator has been published.

SYMBOLS

A	area, cross section
A_{1q}	impeller inlet throat area (trapezoidal: $A_{1q} = a_1 b_1$)
A_{2q}	area between vanes at impeller outlet (trapezoidal: $A_{2q} = a_2 b_2$)
A_{3q}	diffuser inlet throat area (trapezoidal: $A_{3q} = a_3 b_3$)
a	distance between vanes
b	width of vane
b_2	impeller outlet width
c	absolute velocity
c_u	circumferential component of the velocity
c_{3q}	average velocity in diffuser throat $c_{3q} = Q_{Le}/(Z_{Le} A_{3q})$
D, d	diameter
d_{3q}	equivalent diameter of volute throat
d_b	arithmetic average of diameters at impeller or diffuser e.g. $d_{1b} = 0.5 (d_1 + d_{1i})$; defined such that: $A_1 = \pi d_{1b} b_1$
d_m	geometric average of diameters at impeller or diffuser, e.g. $d_{1m} = \sqrt{0.5(d_{1a}^2 + d_{1i}^2)}$
e	vane thickness
g	acceleration due to gravity ($g = 9,81 \text{ m/s}^2$)
H	head
H_p	static pressure rise in impeller
k	rotation of fluid in between impeller and casing
L	length
n	rotational speed (revolutions per minute)
n_q	specific speed (min^{-1} , m^3/s , m)
p	static pressure
p^*	wet perimeter
p_{amb}	ambient pressure
P_d	power dissipation

Q	flow rate, volumetric flow
Q_{La}	flow rate through impeller: $Q_{La} = Q + Q_{sp} + Q_E + Q_h = Q/\eta_v$
Q_{Le}	flow rate through diffuser: $Q_{Le} = Q + Q_{s3} + Q_E$
Q_E	flow rate through axial thrust balancing device
Q_h	flow rate through auxiliaries (mostly zero)
Q_{sp}	leakage flow rate through impeller neck ring
Q_{s3}	leakage flow rate through inter-stage seal
Q^*, q^*	flow rate referred to flow rate at best efficiency point: $q^* = Q/Q_{opt}$
Re	Reynolds number. Channel: $Re = cD_h/\nu$. Blade: $Re = wL/\nu$
R_o	bend radius
r	radius
r_{3q}	equivalent radius of volute throat area
s	gap width
t	pitch $t = \pi d/Z_{La}$ (or Z_{Le})
u	circumferential velocity $u = \pi d n/60$
w	relative velocity
w_{1q}	average velocity in impeller throat area $w_{1q} = Q_{La}/(Z_{La} A_{1q})$
Z_{La}	number of impeller blades
Z_{Le}	number of diffuser vanes (volute: number of cutwaters)
α	angle between direction of circumferential and absolute velocity
α	opening angle of a diffuser
β	angle between relative velocity vector and the negative direction of circumferential velocity
ΔH	hydraulic losses
δ_0	bend angle
ζ	loss coefficient
η_{vol}	volumetric efficiency
θ	angle used for the law section of the spiral casing
λ	angle between vanes and side disks (impeller or diffuser)
ρ	density

ν	kinematic viscosity
τ	vane blockage factor

<i>BEP</i>	Best efficiency point
<i>PAT</i>	Pump as turbine

Subscripts

0	bend
1	impeller blade leading edge (low pressure)
2	impeller blade trailing edge (high pressure)
3	diffuser vane leading edge or volute cutwater
a,m,i	outer, mean, inner streamline
B	blade angle (impeller, diffuser, volute cutwater)
d	discharge nozzle
fr	friction
GC	gradual contraction
GE	gradual expansion
hyd	hydraulic
i	element i of the volute
La	impeller
Le	diffuser
m	meridian component
max	maximum
min	minimum
opt	operation at maximum efficiency (BEP)
r	radial
SC	sudden contraction
SE	sudden expansion
sp	gap, leakage flow
Sp	volute
th	theoretical flow conditions (flow without losses)
tot	total pressure = static pressure + stagnation pressure
u	circumferential component
*	dimensionless quantity: all dimensions are referred to d_2 e.g. : $b_2^* = b_2/d_2$

CONTENTS

1. INTRODUCTION	6
2. STATE OF THE ART	6
3. HYDRAULIC LOSSES IN HYDRAULIC MACHINES.....	7
4. PUMP OPERATION.....	8
4.1 Determination of characteristics in pump operation	9
4.1.1 Euler Head	9
4.1.2 Leakage flow losses.....	10
4.2 Modeling of the complete pump.....	12
4.2.1 Hydraulic losses through the runner	13
4.2.2 Hydraulic losses through the volute	14
4.2.3 Total hydraulic losses.....	16
4.3 Memento of head losses.....	17
4.3.1 Friction losses (ΔH_{fr}).....	17
4.3.2 Sudden contraction and expansion losses ($\Delta H_{SC}, \Delta H_{SE}$)	18
4.3.3 Gradual expansion and gradual contraction losses ($\Delta H_{GE}, \Delta H_{GC}$)	20
4.3.4 Changes of flow direction losses (ΔH_{bend})	23
4.4 Results in pump operation	24
4.4.1 Pumps used	24
4.4.2 Volumetric efficiency	26
4.4.3 Prediction in pump operation	26
5. TURBINE OPERATION	29
5.1 Theoretical head	29
5.2 Leakage flow losses	31
5.3 Model of the hydraulic losses	31
5.4 Prediction of the flow rate at the BEP	33
5.5.Determination of the PAT efficiency	34
5.6 Results in turbine operation	34
5.6.1 Volumetric efficiency	34
5.6.2 Theoretical turbine characteristic	35
5.6.3 Prediction	38
6. EXPLOITATION DU MOTEUR SYNCHROME EN VITESSE VARIABLE	42
7. CONCLUSIONS	43
7.1 Travaux publiés dans le cadre du projet.....	44
7.2 Collaboration nationale	44
8. REFERENCES	44

Appendix.....	45
A.1 The VBA Excel Macro	45

1. INTRODUCTION

In the hydraulic power generation, turbines are built to fit the hydraulic specifications of a site, especially high power turbines. In the case of small sites which generate little power, a very interesting solution, if the efficiency is not primordial, is the use of centrifugal pumps as turbines (PAT). Indeed, a pump slightly modified is a good turbine which reaches a good efficiency. It is also a fact that serial pumps show an interesting cost reduction for a power generation site.

An important application of these pumps as turbines is the energy recovery in water supply systems. If a reverse running pump is installed alongside an energy dissipating valve, most of the dissipated energy can be recovered [15]. Some sewage-treatment outfalls may also have potential for energy recovery using pumps as turbines. For example, a demonstration project built in 1993 in Nyon uses a pump as turbine to produce up to 210 kW electrical power from a sewage outfall [5].

Pumps manufacturers sell their machines with the hydraulic characteristics in pump mode, which have been obtained by experimental tests. Nevertheless they do not know the machine's performances in turbine mode (expensive tests). The main objective of this project is to predict the characteristics of the pump working as a turbine (without any experimental test) thanks to the pump characteristics and the pump geometry.

2. STATE OF THE ART

Several methods have been suggested for predicting the turbine performance based on the data for pump performance at best efficiency, but they produce widely varying results. None of these methods give an accurate prediction for all pumps; at most they just give a first estimate of the turbine performance.

Several authors have published papers on turbine performance prediction using the best efficiency values. In 1962, Childs [6] stated that the turbine best efficiency point and pump best efficiency for the same machines are approximately equal. Stepanoff [14] proposed that the head ratio and the flow rate ratio in turbine and pump operation are in inverse proportion to the pump efficiency square and to the pump efficiency, respectively. Alatorre-Frenk et al.[1] presented formulations based on fitting equations to a limited number of PAT data. Other relations were proposed by Engel [7] and Sharma [13].

Several other authors have published equations that relate the head and flow ratios for pump and turbine operation to the pump or turbine specific speed, see for instance Buse [2], Lewinsky [11] and Grover [8].

Burton et al. [3] have studied the prediction of pumps as turbines using the ratio method, which is a tool for designing centrifugal pumps, whereby the best operating point is determined by the interaction of impeller and volute characteristics. The general equations for impeller and volute characteristics in turbine mode are derived, and they are used to obtain the best operating point.

Rodrigues et al. [12] studied the prediction of a pump as a turbine with CFD and found deviations within 5% to 10% for most of the analyzed parameters (total head, hydraulic torque, hydraulic efficiency).

3. HYDRAULIC LOSSES IN HYDRAULIC MACHINES

Figure 1 shows the types of hydraulic losses which intervene during the pump and turbine operation of a classic centrifugal pump. The losses can be divided in three types:

- 1) A circulation loss in pump operation only, see Figure 1a, which is due to the finite number of blades and which causes a shift of the ideal Euler line.
- 2) Losses proportional to the flow rate (Q^2), see Figure 1b, which can be divided in friction losses when the flow passes through the impeller channels and the casing, and minor or local losses (abrupt changes of section, gradual changes of section, bend effect).
- 3) Incidence or shock losses, see Figure 1c, which occur when there is a misalignment between the direction of flow and the angle of the volute casing and the runner blade angles. This misalignment invokes a residual velocity vector which is the reason for decreasing efficiencies of machines for flows other than the design flow. The BEP flow rate is located near the minimum of the shock losses.

Adding or subtracting all these losses, for turbine and pump respectively, to the ideal Euler line will lead to the actual performance curve.

The two first types of losses will be modeled. These will allow the prediction of the head of the BEP.

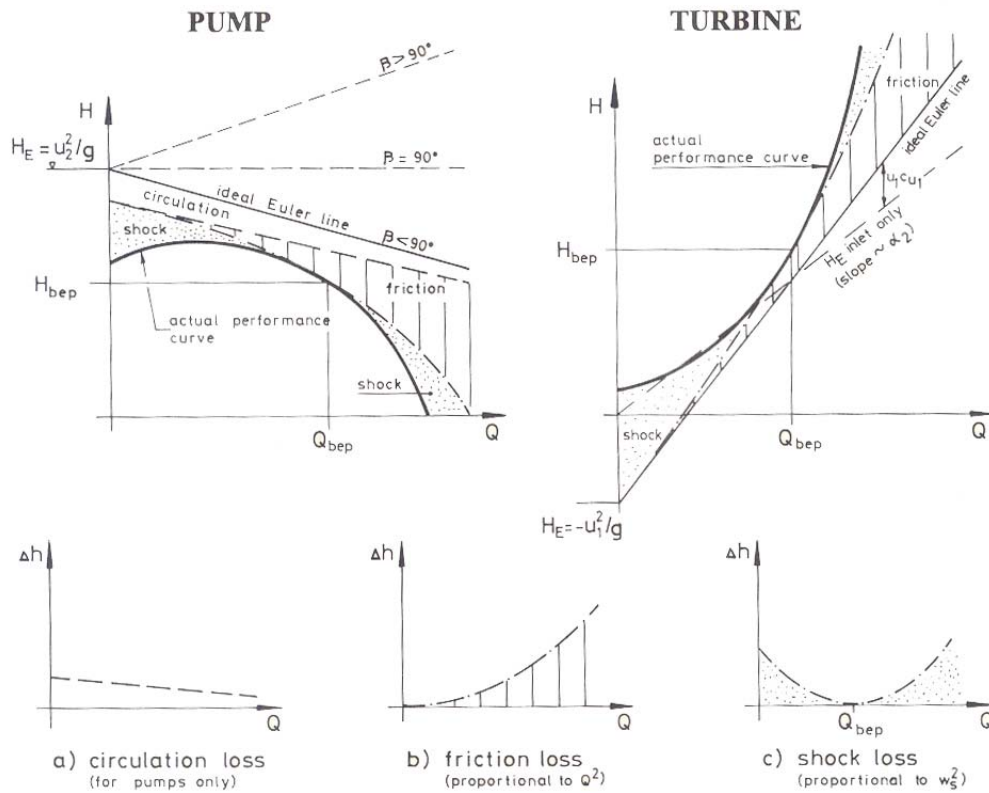


Figure 1: Types of hydraulic losses in a hydraulic turbo-machine [4]

4. PUMP OPERATION

The diagram in Figure 2 shows the procedure followed in this project to determine the curve predictions in pump and in turbine operation. These curves will be compared with experimental data to determine the deviation of head and flow rate for the BEP.

In summary, the starting point for the prediction is to determine the theoretical pump and turbine characteristics (H - Q_{La}) with the help of the pump geometry. Then the loss model proposed is subtracted or added to the pump or turbine theoretical characteristics respectively to get the prediction curves.

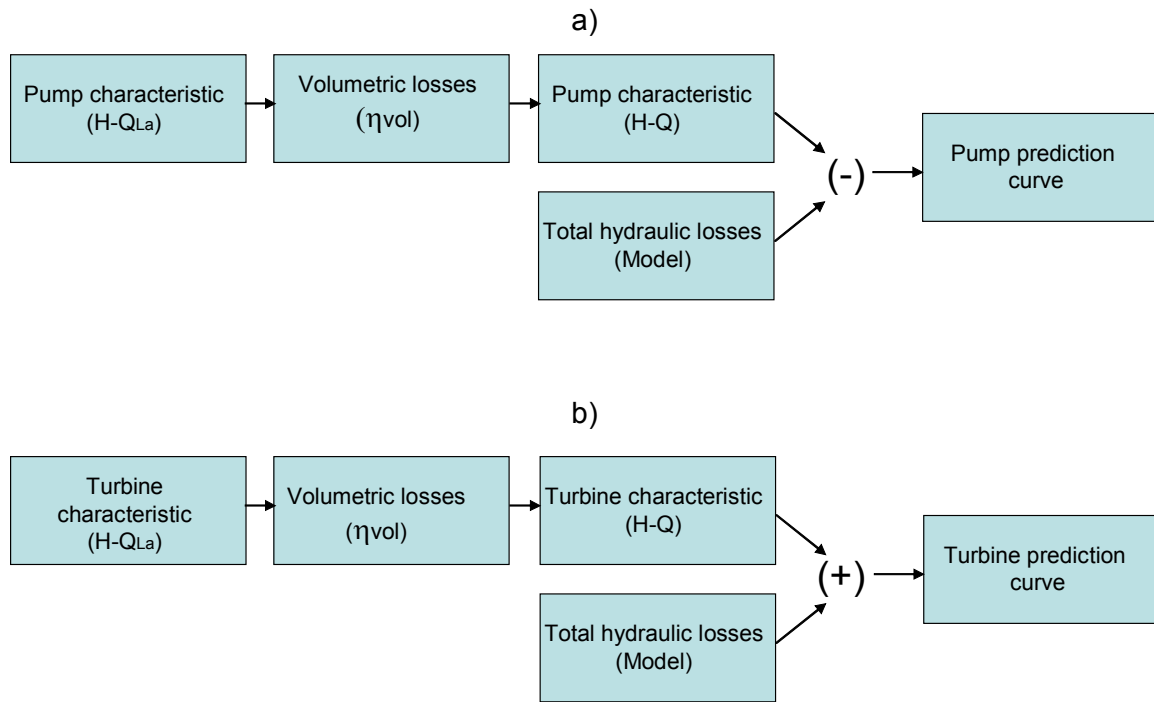


Figure 2 a) Procedure for predicting the pump characteristics (H-Q), b) procedure for predicting the turbine characteristics

4.1 DETERMINATION OF CHARACTERISTICS IN PUMP OPERATION

4.1.1 Euler Head ($H - Q_{La}$)

The fundamental equation for hydraulic machines, the Euler relation, is:

$$gH_{th} = u_2 c_{u2} - u_1 c_{u1} \quad \text{Eq. 1}$$

Under the assumption of a pump with an infinite number of vanes, the theoretical head is written as (for the details of formulas, see Gülich [9]):

$$H_{th-\infty} = \frac{u_2^2}{g} \left\{ 1 - \frac{Q_{La}}{A_2 u_2 \tan \beta_{2B}} \left[1 + \frac{A_2 d_{1m}^* \tan \beta_{2B}}{A_1 \tan \alpha_1} \right] \right\} \quad \text{Eq. 2}$$

The influence of the finite number of vanes (circulation losses) and the vane blockage on the flow can be better represented by adding a factor called the slip factor γ and a blockage factor τ_2 at the pump exit (see Equations 4 and 5).

$$H_{th} = \frac{u_2^2}{g} \left\{ \gamma - \frac{Q_{La}}{A_2 u_2 \tan \beta_{2B}} \left[\tau_2 + \frac{A_2 d_{1m}^* \tan \beta_{2B}}{A_1 \tan \alpha_1} \right] \right\} \quad \text{Eq. 3}$$

where

$$\gamma = f_1 \left(1 - \frac{\sqrt{\sin \beta_{2B}}}{z_{La}^{0.7}} \right) k_w \quad \text{with} \quad \text{Eq. 4}$$

$$k_w = 1 - \left(\frac{d_{1m}^* - \varepsilon_{Lim}}{1 - \varepsilon_{Lim}} \right)^3 \quad \text{and} \quad \varepsilon_{Lim} = \exp \left(- \frac{8.16 \sin \beta_{2B}}{z_{La}} \right)$$

and

$$\tau_2 = \left\{ 1 - \frac{e Z_{La}}{\pi d_2 \sin \beta_{2B} \sin \lambda_{La}} \right\}^{-1} \quad \text{Eq. 5}$$

Note: if an axial flow at the inlet of the pump is assumed, i.e. $\alpha_1 = \pi/2$. The Equation 3 becomes:

$$H_{th} = \frac{u_2^2}{g} \left\{ \gamma - \frac{\tau_2 Q_{La}}{A_2 u_2 \tan \beta_{2B}} \right\} \quad \text{Eq. 6}$$

4.1.2 Leakage flow losses

The pressure difference ΔH_{sp} along the gap for the inwards leakage is (see Figure 3):

$$\Delta H_{sp} = H_p - k^2 \frac{u_2^2}{2g} \left(1 - \frac{d_{sp}^2}{d_2^2} \right) \quad \text{Eq. 7}$$

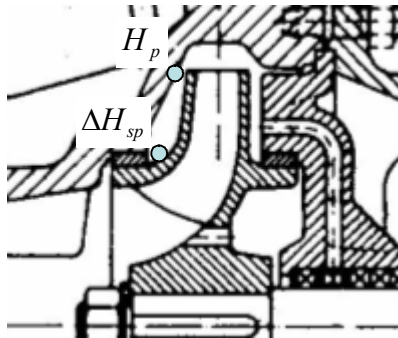


Figure 3: gap for the inwards leakage

with

$$H_p = 0.75H \quad \text{for } n_q < 40$$

$$k = 0.9y_{sp}^{0.087}, \quad y_{sp} = \text{Re}_{u_2}^{0.3} \frac{sd_{sp}}{d_2^2} \sqrt{\frac{s}{L_{sp}}}, \quad \text{Re}_{u_2} = \frac{u_2 r_2}{\nu} \quad \text{Eq. 8}$$

k (rotational factor) representing the rotation of fluid between impeller and casing.

The relation giving the velocity through the gap taking account the number of labyrinths is:

$$c_{ax} = \sqrt{\frac{2g\Delta H_{sp}}{\zeta_{EA} + \lambda \frac{L_{sp}}{2s} + \sum_i \left(\frac{d_{sp}}{d_{si}} \right)^2 \left(\frac{s}{s_i} \right)^2 \left(\zeta_k + \lambda_i \frac{L_i}{2s_i} \right)}} \quad \text{Eq. 9}$$

In order to calculate the head loss coefficient $\lambda = \lambda(\text{Re})$ and then the axial velocity c_{ax} along the gap, a recursive method is applied as follows:

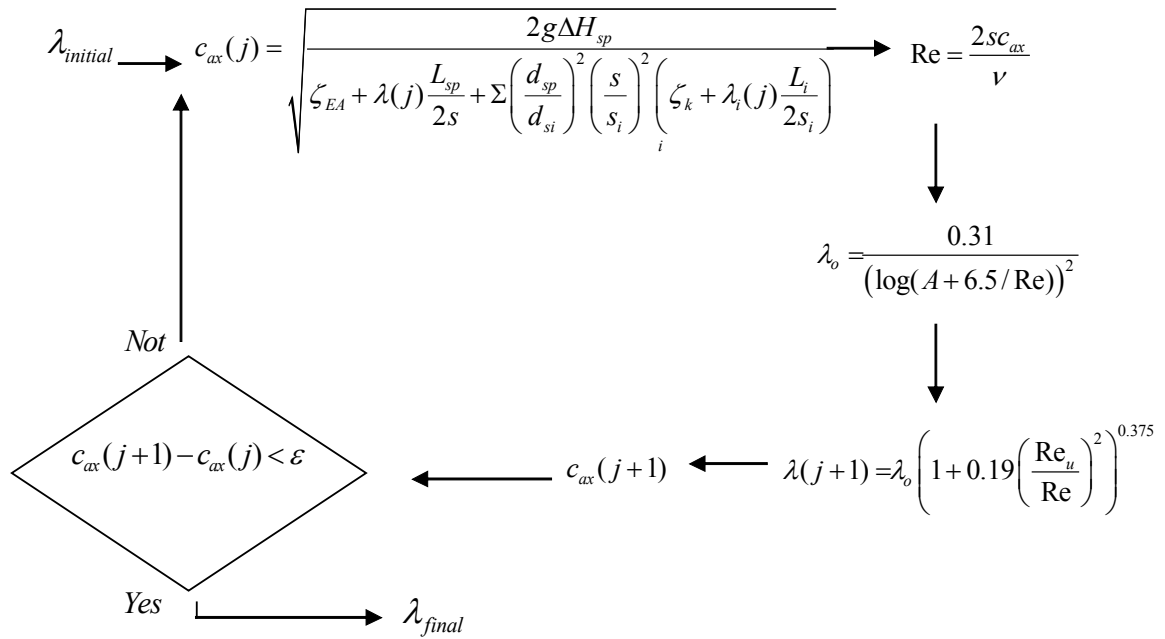


Figure 4: Loop to calculate the head loss coefficient and then the axial velocity through the gap

Where λ_o is the loss coefficient for turbulent flow and $\lambda(j+1)$ is the loss coefficient taking into account the impeller rotation (fluid particle goes a longer distance).

The flow rate Q_{sp} through the gap is:

$$Q_{sp} = \pi d_{sp} s c_{ax} \quad \text{Eq. 10}$$

Finally the pumping volumetric efficiency is:

$$\eta_v = \frac{Q}{Q_{La}} = \frac{Q}{Q + Q_{sp}} \quad \text{Eq. 11}$$

The head H_{th} shown in Eq. 6 is function of Q_{La} , the flow rate flowing through the impeller. By taking into account the leakage losses calculated according to Eq. 10, the head can be written in function of Q , the flow rate through the machine, as:

$$H_{th} = \frac{u_2^2}{g} \left\{ \gamma - \frac{\tau_2 Q / \eta_v}{A_2 u_2 \tan \beta_{2B}} \right\} \quad \text{Eq. 12}$$

All pump characteristics in this study will be represented in function of Q which is obtained thanks to the volumetric efficiency η_v .

4.2 MODELING OF THE COMPLETE PUMP

The pump can be modeled as a set of elements or channels connected in series and parallel from its inlet to its exit.

Figure 5 shows a simplified scheme with the main hydraulic losses (friction and minor losses) in the impeller and in the volute in pump mode.

The assumptions for the pump model used are: constant static pressure around the inlet and outlet diameter of the runner (d_1 and d_2) and uniform pressure through section D_d (discharge nozzle). These assumptions are at least true near to the best operating point.

These assumptions imply the same energy losses through each runner channel and through each volute channel (if pump with double volute).

Then, the runner is modeled as a set of channels in parallel representing the lines of head losses according to the number of vanes. The volute is also modeled in 2 parallel lines (if double volute).

Thus the total head losses are obtained by the sum of head losses through only one runner channel and through only one volute channel.

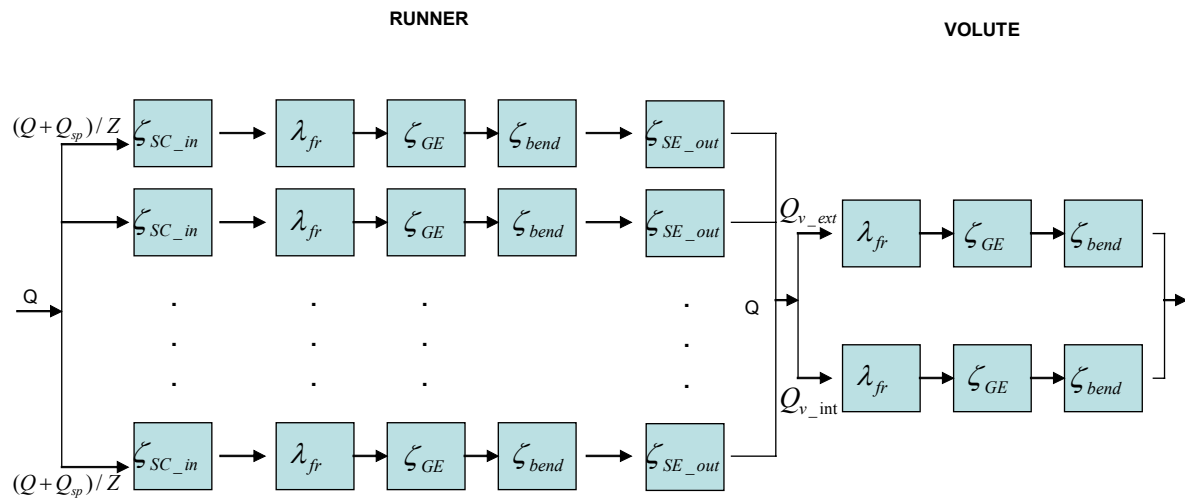


Figure 5: scheme for the model of the hydraulic losses in a pump

Losses through the pump channels are obtained with the help of relations well known for friction and minor losses. The channels and sections of the pump have been decomposed in simple elements in order to be able to use the Idel'cik [10] relations.

4.2.1 Hydraulic losses through the runner

According to the principle of superposition of losses, every channel in the runner is submitted to 3 types of losses: friction losses ΔH_{fr} , bend losses ΔH_{bend} and gradual expansion losses in pump mode ΔH_{GE} or gradual contraction losses in turbine mode ΔH_{GC} .

Figure 6 shows a representation of one runner channel in which an average path of length L_m has been determined with the help of balls following the channel form. The curve angle of the path is δ_0 and the radius R_0 . To see the determination of those parameters refer to Figures 31, 33, 35, 37 in Appendix.

An important parameter to calculate the losses is the hydraulic diameter D_H defined as:

$$D_H = \frac{4A}{p^*} \quad \text{Eq. 13}$$

with the wet perimeter p^* and the blocked exit or throat area A (A_{1q} and A_{2q} in Figure 8).

Since the hydraulic diameter varies along the vanes, a weighted average is used for the calculation

$$D_{HEQ} = \frac{D_{H1} + 2\bar{D}_H + D_{H2}}{4} \quad \text{Eq. 14}$$

where

$\bar{D}_H$ is the hydraulic diameter at midpoint.

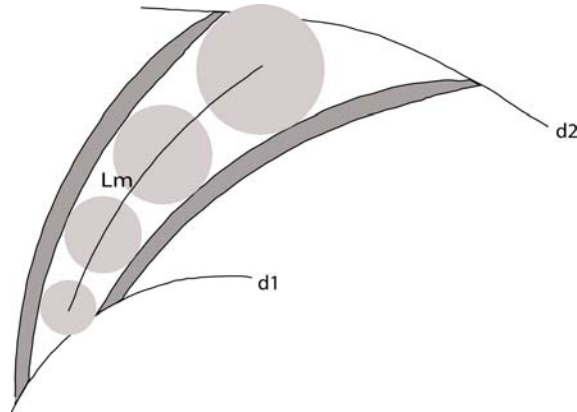


Figure 6: Representation for the modeling of a runner channel

4.2.2 Hydraulic losses through the volute

The volute is divided into elements according to the volute angle θ_i ($0 < \theta_i < 360^\circ$) which starts at the cutwater at $\theta_1 = 0^\circ$ (Figure 7). The diffuser part at the volute outlet can also be divided into several elements.

As was done for the runner, friction losses, bend losses and gradual expansion or contraction losses for each element can be added and a total head loss in the volute determined.

In the case of a double volute there are two cutwaters. Thus the volute is divided into two channels. Each channel can be divided into elements in which losses can be determined.

For each element of the volute, the hydraulic diameter can be determined with the help of cross sections of the volute and with the wet perimeters (see also Figures 32, 34, 36, 38 in Appendix). The path length and the radius curve for each element help to determine losses according to section 5.3.

To determine the distribution of the flow rate through each channel of the double volute, two lines where the total head loss in each "leg" is identical (Eq. 19) are considered (Figure 7).

$$gH_{r_InnerLeg} = gH_{r_OuterLeg} \quad \text{Eq. 15}$$

and the coefficients K characterizing the losses which are function of Q^2 are:

$$K_{outer} = \frac{H_{r_OuterLeg}}{Q_{outer}^2}, \quad K_{inner} = \frac{H_{r_InnerLeg}}{Q_{inner}^2} \quad \text{Eq. 16}$$

The function relative to Q_{inner} to minimize and obey the Eq. 15 is:

$$f(Q_{inner}) = K_{inner}Q_{inner}^2 + K_{outer}(Q - Q_{inner})^2 \quad \text{Eq. 17}$$

In order to attain same head losses in each leg, iterations are performed while the flow through the two legs is altered (respecting the law of continuity $Q_{tot} = Q_{inner} + Q_{outer}$).

Using Taylor's method to calculate the flow rate across the inner leg Q_{inner} , which minimizes Eq. 17, it becomes:

$$\begin{cases} Q_{inner_init} = \frac{\theta_{inner}}{360} Q \\ Q_{inner}(i+1) = Q_{inner}(i) - \frac{f(Q_{inner})}{f'(Q_{inner})} \end{cases} \quad \text{Eq. 18}$$

The calculation stops after the convergence condition $f(Q_{inner}) < \varepsilon$ is reached.

4.2.3 Total hydraulic losses

The relation leading to the total hydraulic losses of the pump is showed in Eq. 19.

$$\Delta H_{Total_Loss} = (\Delta H_{fr} + \Delta H_{GE/GC} + \Delta H_{SE/SC})_{runner} + \sum_i^n (\Delta H_{fr} + \Delta H_{GE/GC} + \Delta H_{SE/SC})_{volute} \quad \text{Eq. 19}$$

where n is the number of elements in which the volute has been divided.

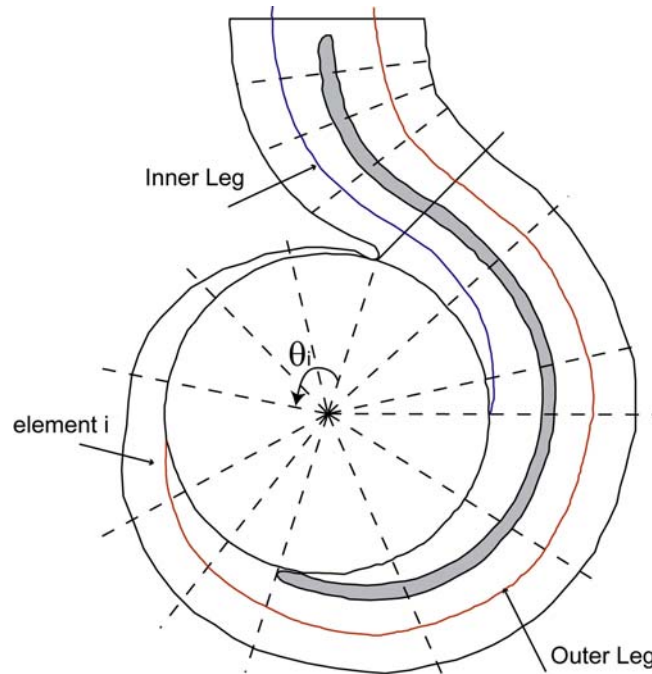


Figure 7: Division of the volute into elements according to the angular position

4.3 MEMENTO OF HEAD LOSSES

4.3.1 Friction losses (ΔH_{fr})

The head friction loss in a pipe is:

$$\Delta H_{fr} = \frac{\lambda L}{D_H} \frac{c^2}{2g} \quad \text{Eq. 20}$$

with the friction factor λ calculated as:

$$\lambda = \frac{0.3086}{\left[\log_{10} \left(0.135 * \bar{\Delta} + \frac{6.5}{\text{Re}} \right) \right]^2} \quad \text{Colebrook's formula} \quad \text{Eq. 21}$$

and the relative roughness coefficient $\bar{\Delta} = (\Delta / D_H)$.

In order to calculate the friction losses in the spiral parts of the volute which are not closed tubes, we considered them as flat plates and a dissipation coefficient on a flat plate is used:

$$c_f = \frac{0.13}{\left(\log_{10} \left(0.135 \frac{\varepsilon}{\Delta L} + \frac{6.5}{\text{Re}} \right) \right)^2} \quad \text{Eq. 22}$$

Because this open part of spiral has been divided in several elements placed one after the other, it can be considered as a serial circuit in which the total loss coefficient can be defined as:

$$\zeta_{sp} = \zeta_1 \left(\frac{A_{ref}}{A_1} \right)^2 + \zeta_2 \left(\frac{A_{ref}}{A_2} \right)^2 + \zeta_3 \left(\frac{A_{ref}}{A_3} \right)^2 + \dots = \sum \zeta_i \left(\frac{A_{ref}}{A_i} \right)^2 \quad \text{Eq. 23}$$

where A_{ref} is a reference section and A_i is the cross section of the element i . In the double volute the reference sections are the throat areas near to the two cutwaters.

The total loss head is:

$$gH_{sp} = \frac{\zeta_{sp}}{2} \left(\frac{Q}{A_{ref}} \right)^2 \quad \text{Eq. 24}$$

The power dissipation for one element of the spiral is:

$$dP_d = c_f \frac{\rho}{2} c^3 dA \text{ with } dA = dU \cdot dL \quad \text{Eq. 25}$$

where c is the mean velocity in the element i and proportional to the flow rate Q_i varying through the spiral. The total head loss can be written:

$$gH_{sp} = \frac{P_d}{\rho Q} \quad \text{Eq. 26}$$

where P_d is the total power dissipation.

Using Eq. 23 to Eq. 26, the total head loss coefficient can be pointed out:

$$\zeta_{sp} = \frac{2P_d}{\rho c_{ref}^3 A_{ref}} \quad \text{Eq. 27}$$

Finally gH_{sp} , the total head loss in the spiral part of the volute which is not closed, is determined with Eq. 24.

4.3.2 Sudden contraction and expansion losses ($\Delta H_{SC}, \Delta H_{SE}$)

Sudden contraction and expansion losses occur at the inlet and at the exit of the runner channels in both pump and turbine modes.

The areas used to calculate these losses are those called throat area or blocked area A_{1q}, A_{2q} (taken normal to the vanes), see Figure 8.

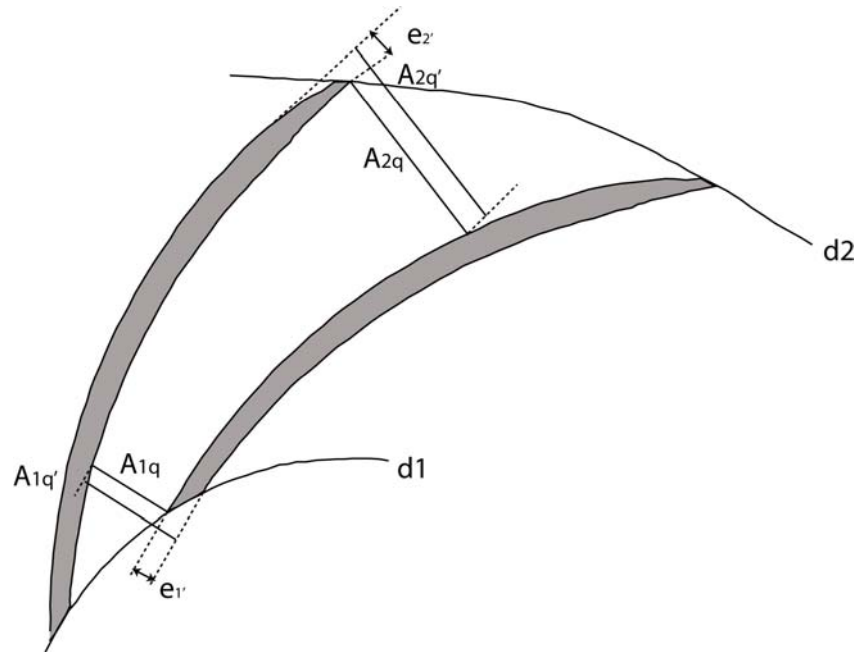


Figure 8: Areas used to calculate the sudden expansion and contraction losses in the runner

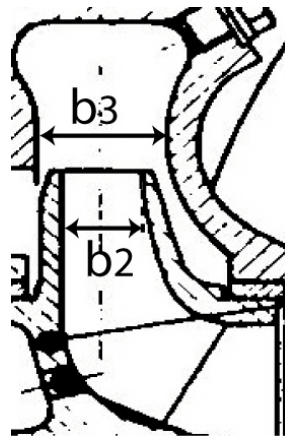


Figure 9: Dimensions to calculate sudden expansion or contraction between the volute and the runner

The relations used to calculate the sudden contraction losses and the sudden expansion losses in pump mode are:

$$\Delta H_{SC} = \zeta_{SC} \frac{c^2}{2g}, \quad \Delta H_{SE} = \zeta_{SE} \frac{c^2}{2g} \quad \text{Eq. 28}$$

The sudden contraction losses coefficient ζ_{SC} and the sudden expansion losses coefficient ζ_{SE} in pump mode are (see Idel'cik [10]):

$$\zeta_{SC} = 0.5 \left(1 - \frac{A_{1q}}{A_{1q'}} \right) \quad \text{Eq. 29}$$

$$\zeta_{SE1} = \left(1 - \frac{A_{2q}}{A_{2q'}} \right)^2 \quad \text{Eq. 30}$$

$$\zeta_{SE2} = \left(1 - \frac{A_{2q''}}{A_{3q'}} \right)^2 \quad \text{Eq. 31}$$

with:

$$A_{1q} = a_1 b_1$$

$$A_{1q'} = (a_1 + e_1) b_1$$

$$A_{2q} = a_2 b_2$$

$$A_{2q'} = (a_2 + e_2) b_2 \quad \text{Eq. 32}$$

$$A_{2q''} = \left(\frac{2\pi r_2}{Z_{La}} - e_2 \right) b_2$$

$$A_{3q'} = \left(\frac{2\pi r_2}{Z_{La}} - e_2 \right) b_3$$

Note: The same relations are used also to calculate the sudden expansion and contraction losses in turbine mode, taking account of the flow direction.

4.3.3 Gradual expansion and gradual contraction losses (ΔH_{GE} , ΔH_{GC})

The volute has parts which behave as diffusers, for instance the discharge part at the volute outlet. In order to calculate the loss coefficient in a diffuser, experimental pressure recovery coefficient curves are used as shown in Figure 10.

The recovery coefficient of a diffuser (1: inlet section, 2: outlet section) is defined as:

$$c_p = \frac{p_2 - p_1}{\rho \frac{c_1^2}{2}} = \left(\frac{c_2}{c_1} \right)^2 - 1 + \frac{gH_{r1 \rightarrow 2}}{\frac{c_1^2}{2}} \quad \text{Eq. 33}$$

and the head loss is:

$$H_{r1 \rightarrow 2} = \frac{1}{2} \frac{c_1^2}{g} \left(1 - c_p - \left(\frac{A_1}{A_2} \right)^2 \right) \quad \text{Eq. 34}$$

The loss coefficient in a diffuser is:

$$\zeta_D = 1 - c_p - \left(\frac{1}{A_R} \right)^2 \quad \text{Eq. 35}$$

where

$$A_R = \frac{A_2}{A_1} \quad \text{Eq. 36}$$

In Figure 10, N / R_1 is the non-dimensional length of the diffuser.

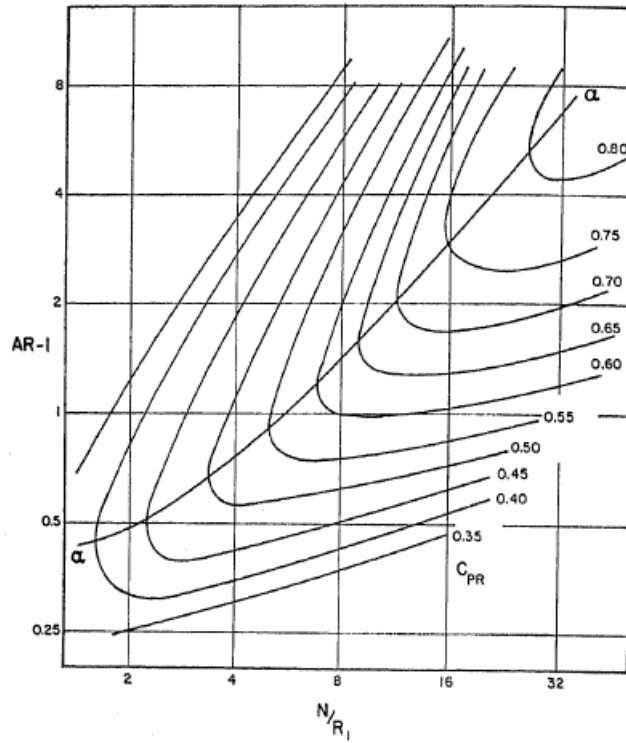


FIG. 13. Pressure recovery contours cross-plotted from conical diffuser data.

Figure 10: Experimental curves of the pressure recovery diffuser [16]

Gradual expansion losses occur through the runner channels and through the volute channels in pump mode.

Gradual contraction losses occur in the runner channels and in the volute channels in turbine mode.

The relations used to determine these losses are:

$$\Delta H_{GE} = \zeta_{GE} \frac{c^2}{2g} \text{ and } \Delta H_{GC} = \zeta_{GC} \frac{c^2}{2g} \quad \text{Eq. 37}$$

The gradual expansion coefficient is determined as (see Idel'cik [10]):

$$\zeta_{GE} = 3.2 \left(\tan \frac{\alpha}{2} \right)^{1.25} \left(1 - \frac{A_m}{A_{out}} \right)^2 \quad \text{for } 0 < \alpha < 40^\circ \quad \text{Eq. 38}$$

There are no empirical equations for the gradual contraction coefficient ζ_{GC} but tables for different opening angles and section ratios can be found in the literature. In our study, these losses are not considered because of the small angles of contraction.

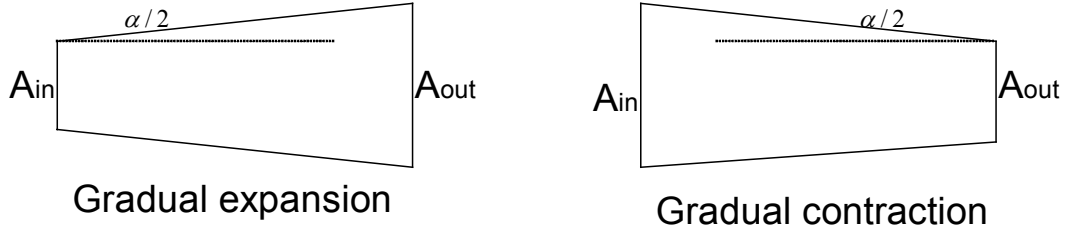


Figure 11: gradual expansion and contraction losses

4.3.4 Changes of flow direction losses (ΔH_{bend})

The losses due to the bend geometry occur in the runner and along the volute, for pump and turbine operation and are written as:

$$\Delta H_{bend} = \zeta_{bend} \frac{c^2}{2g} \quad \text{Eq. 39}$$

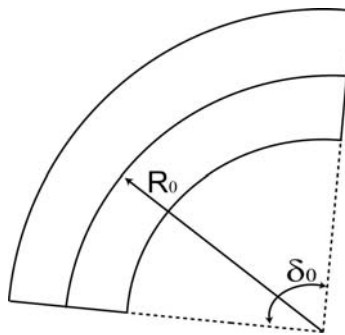


Figure 12: bend losses

The coefficient of bend losses is (see Idel'cik [10]):

$$\zeta_{bend} = A_1 B_1 C_1 \quad \text{Eq. 40}$$

where

$$A_1 = 1.6348 \cdot 10^{-7} \delta^3 - 8.1581 \cdot 10^{-5} \delta^2 + 1.714185 \cdot 10^{-2} \delta \quad \text{Eq. 41}$$

$$B_1 = \begin{cases} \frac{0.21}{\left(\frac{R_o}{D_H}\right)^{2.5}} & \text{for } 0.5 \leq \frac{R_o}{D_H} \leq 1 \\ \frac{0.21}{\left(\frac{R_o}{D_H}\right)} & \text{for } \frac{R_o}{D_H} > 1 \end{cases} \quad \text{Eq. 42}$$

C_1 depends on the ratio of a_o/b_o . For square and circular sections: $C_1 = 1$.

4.4 RESULTS IN PUMP OPERATION

4.4.1 Pumps used

Five pump geometries have been used to test the model proposed. The main characteristics of these pumps are shown in Table 1.

Pump No 1, a pump from Biral, belongs to the EIG. A test rig has been built in the hydraulic laboratory in order to measure the pump and turbine characteristics (head, efficiency and power output). Because the geometry of the Biral pump was not known, it has been dismantled and measurements of the runner and of the volute have been performed, see Figures 12a to 12c.

The plans of the four other geometries were provided by Sulzer with their respective measured characteristics as pumps and as turbines.

Pump No	Specific speed (n_q)
1 (Pump from Biral, EIG)	40
2 Sulzer	19
3 Sulzer	28.7
4 Sulzer	26.7
5 Sulzer	31.6

Table 1: Some specifications of pumps used in the project

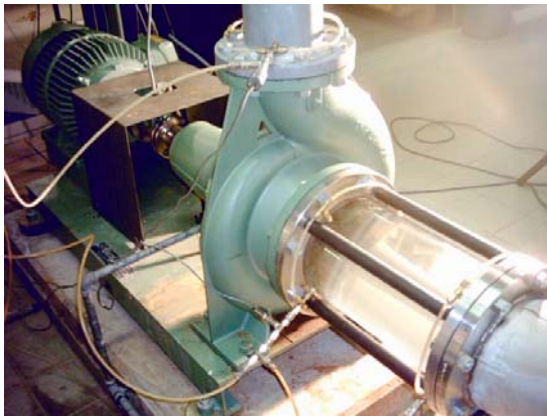


Figure 12a): Test rig of PAT at the EIG (Biral pump) measurements



Figure 12b): Volute geometry measurements

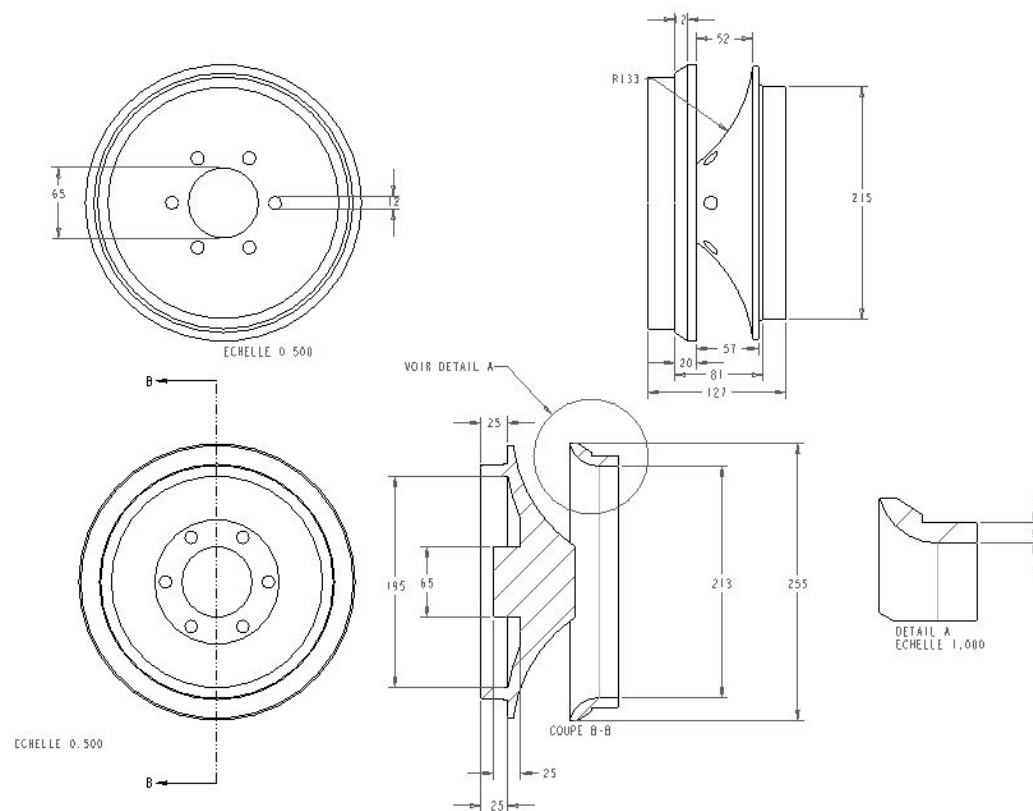


Figure 12c): Geometry of the runner of the Biral pump measured by the EIG

4.4.2 Volumetric efficiency

Figure 13 shows the results of the volumetric efficiency modeling for the four pumps according to the flow rate.

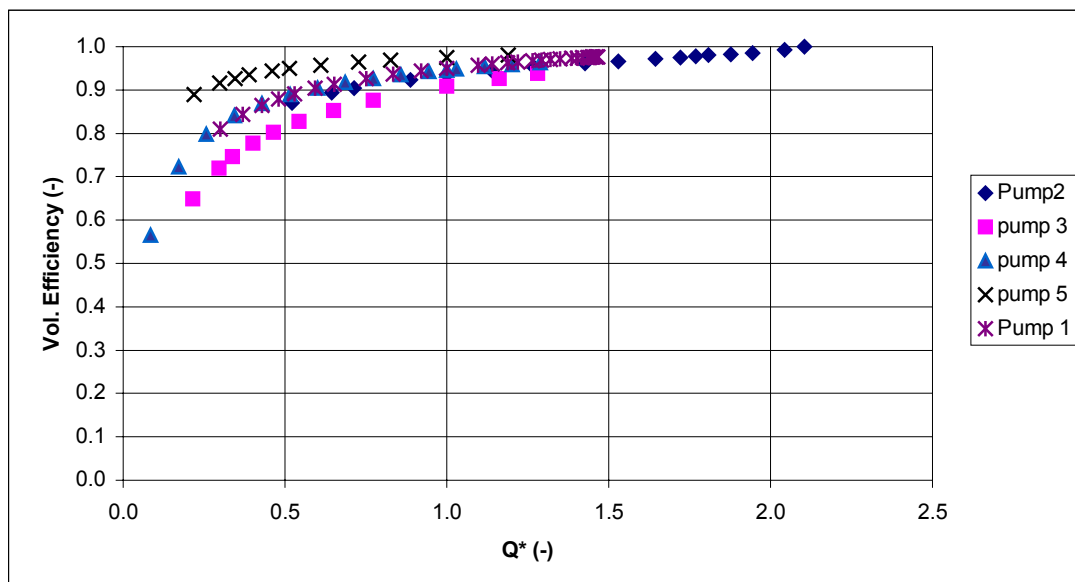


Figure 13: volumetric efficiency modeling

4.4.3 Prediction in pump operation

Figures 14 to 18 show the characteristics (H-Q) predicted in pump mode, the total head losses modeled (related to Q^2) and the experimental pump curve provided by Sulzer.

Table 2 shows the relative differences between the head predicted and the head measured at the BEP.

	H* predicted (-)	Relative error (%)
No 1		
No 2	1.048	4.8
No 3	1.048	4.8
No 4	1.063	6.3
No 5	0.983	-1.65

TABLE 2: Relative error between the prediction and the measurement

It is observed that the predicted pump characteristics curves fit the experimental data very well in the zone near to the BEP. Deviations from 1% to 5% between the predicted head and the head measured at BEP are obtained for the tested pumps.

No correction has been applied to the model of head losses to fit the experimental results. As conclusion we can say that the model proposed can be used for the prediction in turbine operation following the same approach.

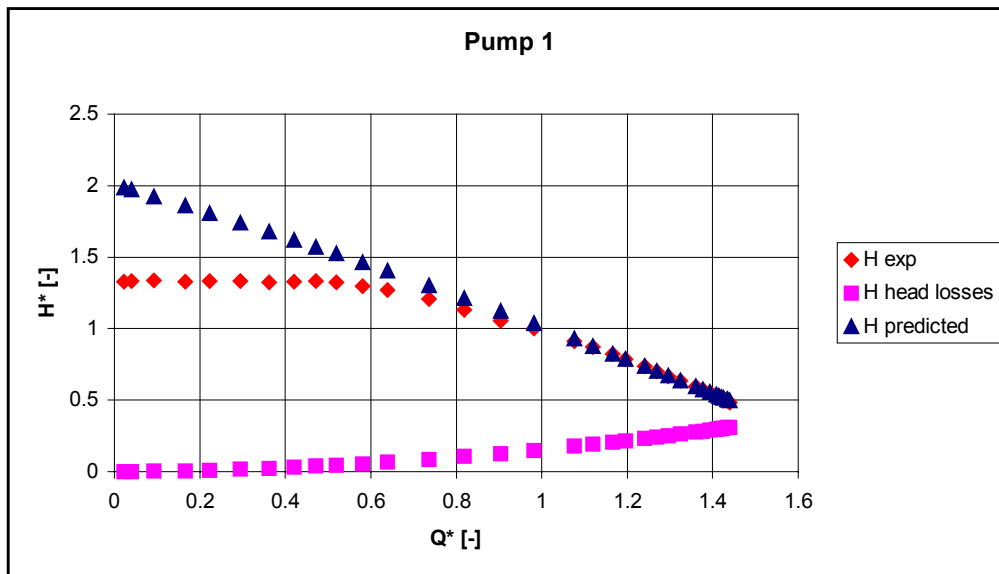


Figure 14: Comparison between the measurements and the prediction in pump operation (pump 1)

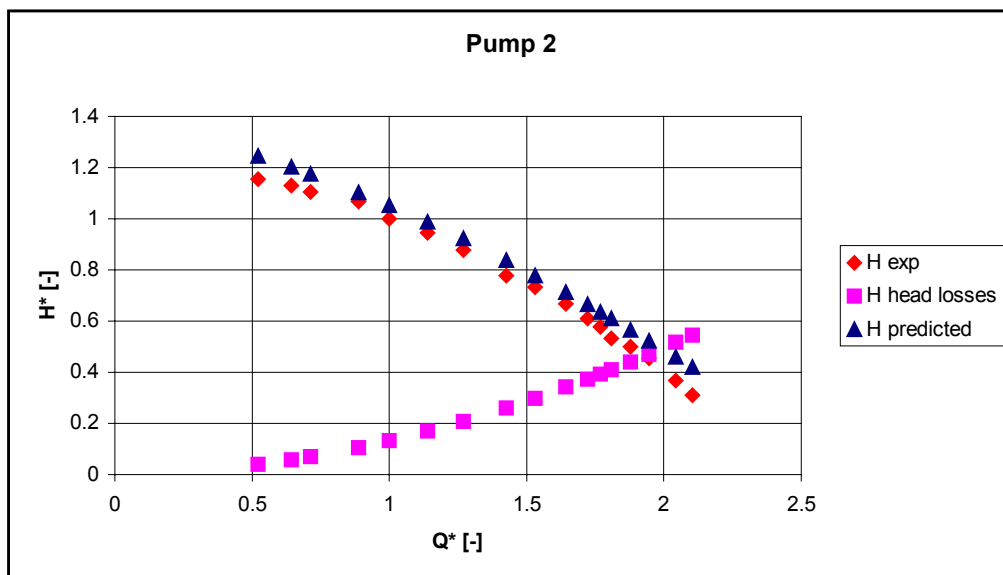


Figure 15: Comparison between the measurements and the prediction in pump operation (pump 2)

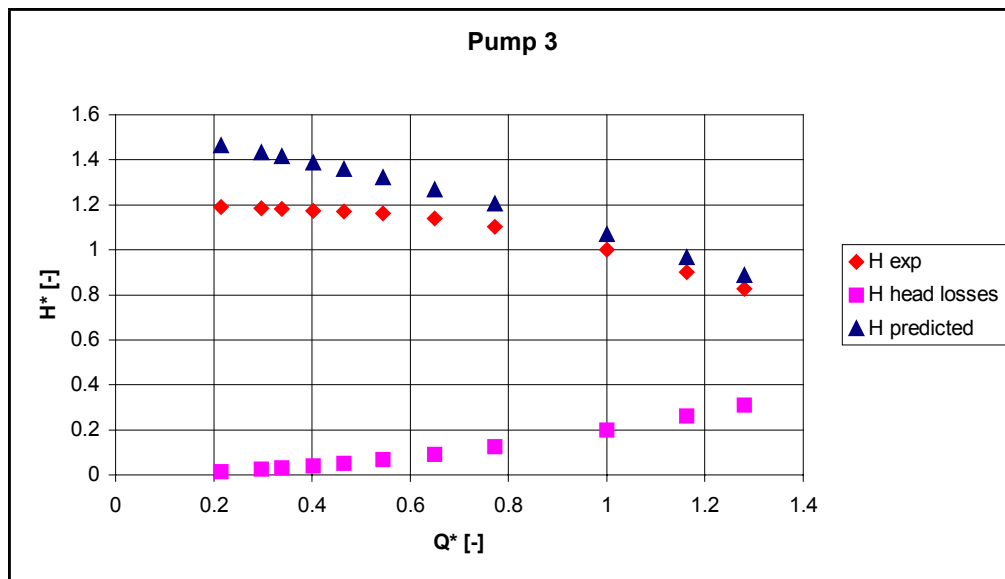


Figure 16: Comparison between the measurements and the prediction in pump operation (pump 3)

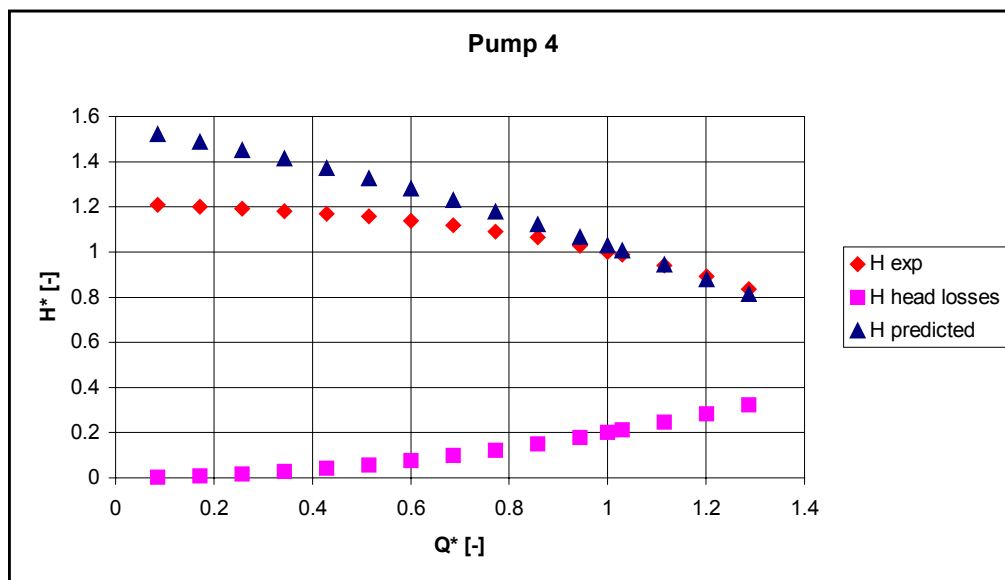


Figure 17: Comparison between the measurements and the prediction in pump operation (pump 4)

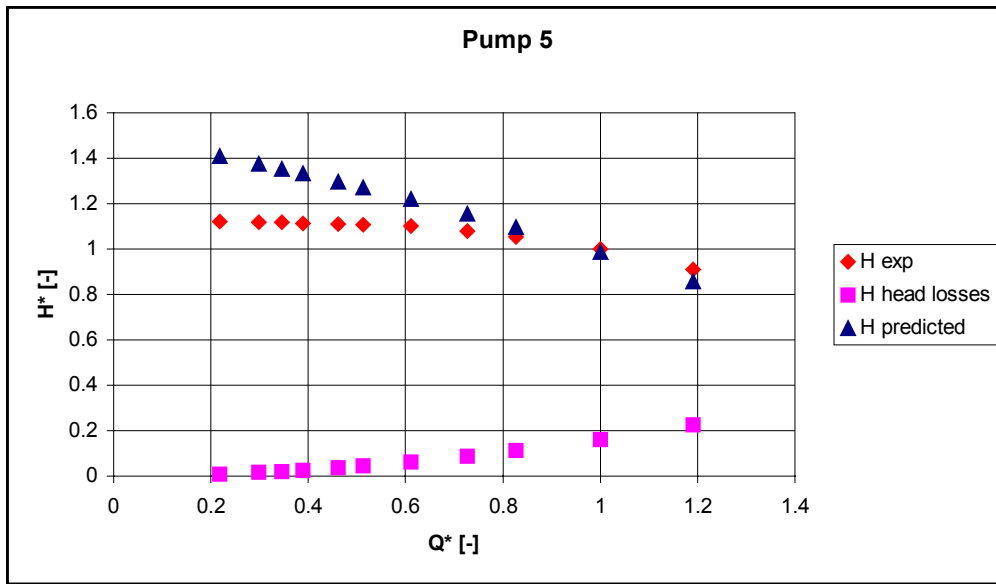


Figure 18: Comparison between the measurements and the prediction in pump operation (pump 5)

5. TURBINE OPERATION

5.1 THEORETICAL HEAD

From the general equation of turbo machines, Eq.43 can be determined for a hydraulic turbine (more details in Gulich [9]).

$$gH_{th} = u_2 c_{u2} - u_1 c_{u1} = \frac{u_2 c_{m2}}{\tan \alpha_2} + \frac{u_1 c_{m1}}{\tan \beta_1} - u_1^2 \quad \text{Eq. 43}$$

where:

$$\tan \alpha_2 = \frac{c_{m2}}{c_{u2}} \quad \text{Eq. 44}$$

The inflow angle α_2 at turbine inlet can be determined from the casing geometry with the help of the blocked cross section A_{q3} , as follows (see also Figure 19).

$$\alpha_{B3} = \arcsin \frac{a_3}{t_3} \quad \text{Eq. 45}$$

$$c_{u3} = c_{q3} \cos \alpha_{B3} \text{ and } c_{q3} = \frac{Q}{A_{q3}} \quad \text{Eq. 46}$$

For a double volute, A_{q3} is obtained by the sum of the two blocked sections.

Finally :

$$c_{u2} = \frac{d_3}{d_2} c_{u3} \quad \text{Eq. 47}$$

The flow angle β_1 can be determined from the runner geometry at outlet:

$$\tan \beta_1 = \frac{z_{La} A_{q1}}{\cos \beta_{A1} A_1} \quad \text{Eq. 48}$$

where

$$\beta_{A1} = \arcsin \frac{A_{1q}}{b_1 t_1} \quad \text{Eq. 49}$$

For the calculation of the geometrical parameters of the volute, a representation of the unfolded volute can be drawn (see Figure 19).

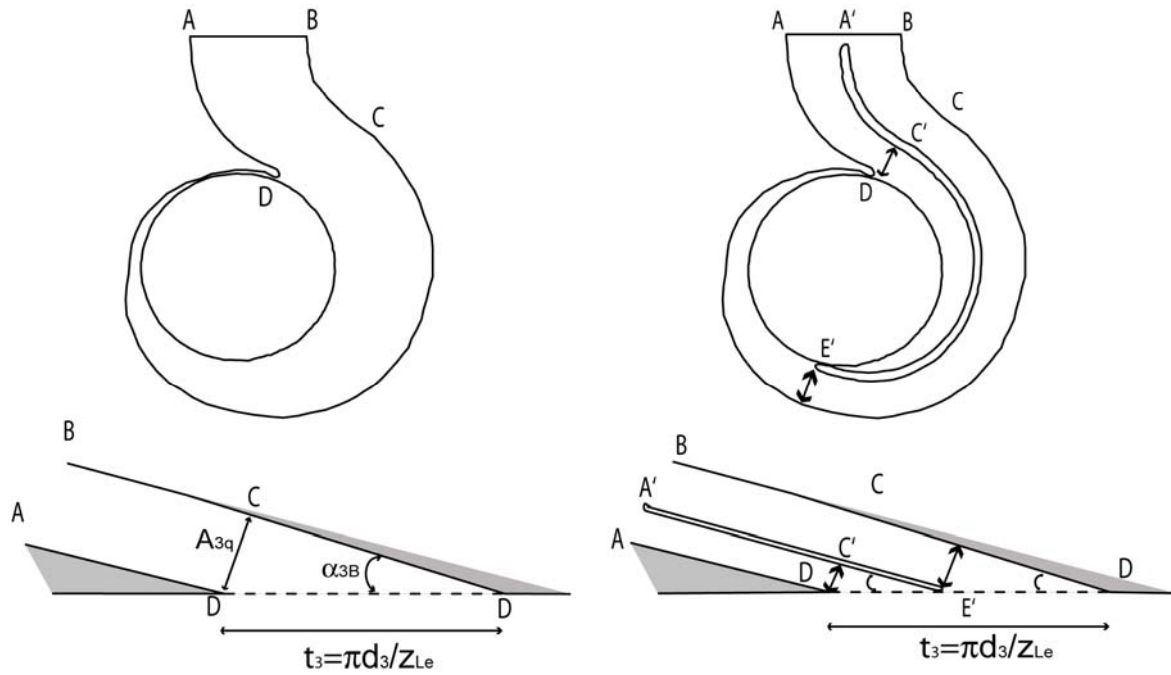


Figure 19: simple volute and double volute with their unfolded representations to determine α_{3B}

5.2 LEAKAGE FLOW LOSSES

In turbine mode, Equations 7 to 10 can be used to calculate the flow leakages Q_{sp} , taking into account that at this time the flow rate through the runner Q_{La} is:

$$Q_{La} = Q - Q_{sp} \quad \text{Eq. 50}$$

The volumetric efficiency in turbine operation is:

$$\eta_v = \frac{Q_{La}}{Q} = \frac{Q - Q_{sp}}{Q} \quad \text{Eq. 51}$$

5.3 MODEL OF THE HYDRAULIC LOSSES

As done for pumps, the head losses in turbine operation are obtained with the help of the relations for friction and minor losses presented in Chapter 5. The channels and sections of the runner and of the casing have been decomposed into simple elements in order to be able to use the Idel'cik [10] relations.

Figure 20 shows the decomposition of the runner and of the casing. Following the flow direction in turbine operation, the casing is considered as two channels in parallel (double volute) and the runner is considered as channels in parallel according to the number of vanes.

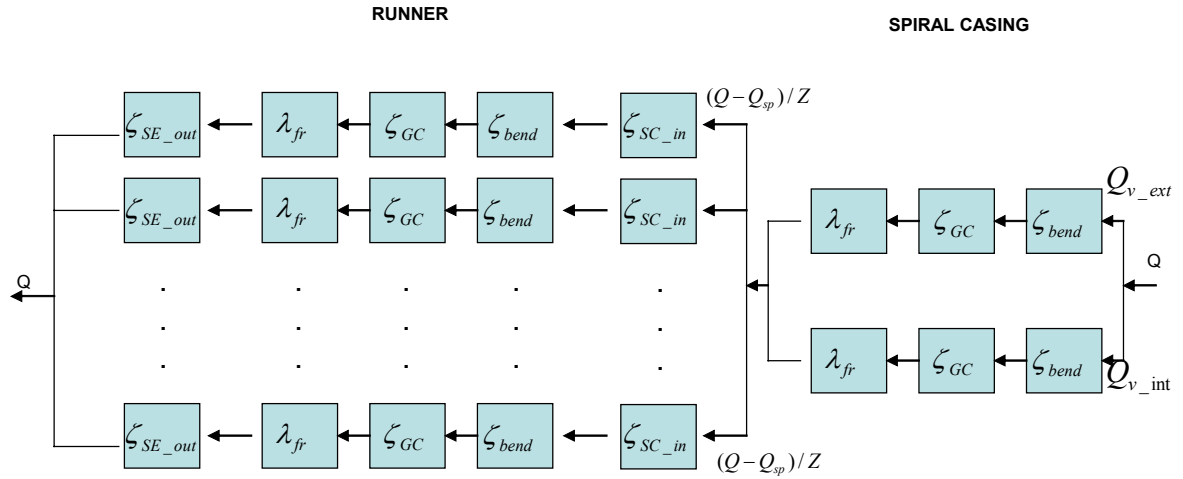


Figure 20: scheme for the model of the hydraulic losses in a turbine

The distribution of the flow rate between the channels of the volute in turbine operation depends on the resistance met by the flow, the flow distribution in turbine operation does not follow any law.

To determine the distribution of the flow in the casing (for a double volute) an energy balance between the inlet of the casing and the outlet of the runner is performed. Considering that energy losses through each channel of the runner are the same and that the energy losses at the interface runner-casing are uniform (at least at the BEP), we reach the conclusion that the losses are the same in each channel of the volute.

Then, the assumption is (like in Eq. 15):

$$gH_{r \text{ Inner } 1 \rightarrow 2} = gH_{r \text{ outer } 1 \rightarrow 2} \quad \text{Eq. 52}$$

At the inner leg:

$$\begin{aligned} gH_{\text{Inner}1} &= gH_{\text{Inner}2} + gH_{r1 \rightarrow 2} \\ \frac{p_{\text{Inner}1}}{\rho} + \frac{c_{\text{Inner}1}^2}{2} &= \frac{p_{\text{Inner}2}}{\rho} + \frac{c_{\text{Inner}2}^2}{2} + gH_{r \text{ Inner } 1 \rightarrow 2} \end{aligned} \quad \text{Eq. 53}$$

At the outer leg:for

$$\begin{aligned} gH_{\text{Outer}1} &= gH_{\text{Outer}2} + gH_{r1 \rightarrow 2} \\ \frac{p_{\text{Outer}1}}{\rho} + \frac{c_{\text{Outer}1}^2}{2} &= \frac{p_{\text{Outer}2}}{\rho} + \frac{c_{\text{Outer}2}^2}{2} + gH_{r \text{ outer } 1 \rightarrow 2} \end{aligned} \quad \text{Eq. 54}$$

The distribution condition of the flow rate through each channel is:

$$\left(\frac{Q_{\text{Inner}}}{Q_{\text{Outer}}} \right)^2 = \frac{K_{\text{Inner}}}{K_{\text{Outer}}} \quad \text{Eq. 55}$$

where K is the total coefficient characterizing the total head losses function of Q^2 .

5.4 PREDICTION OF THE FLOW RATE AT THE BEP

The prediction of the flow rate depends on the determination of the shock losses which appear off the BEP. The behaviour of these losses is bad known and very few researches have been done about that. That is why it has been decided to use a statistical method to determine the flow rate at the BEP. The Chapallaz method (the curve at Fig. 21) have shown a very good accurate at low specific speed.

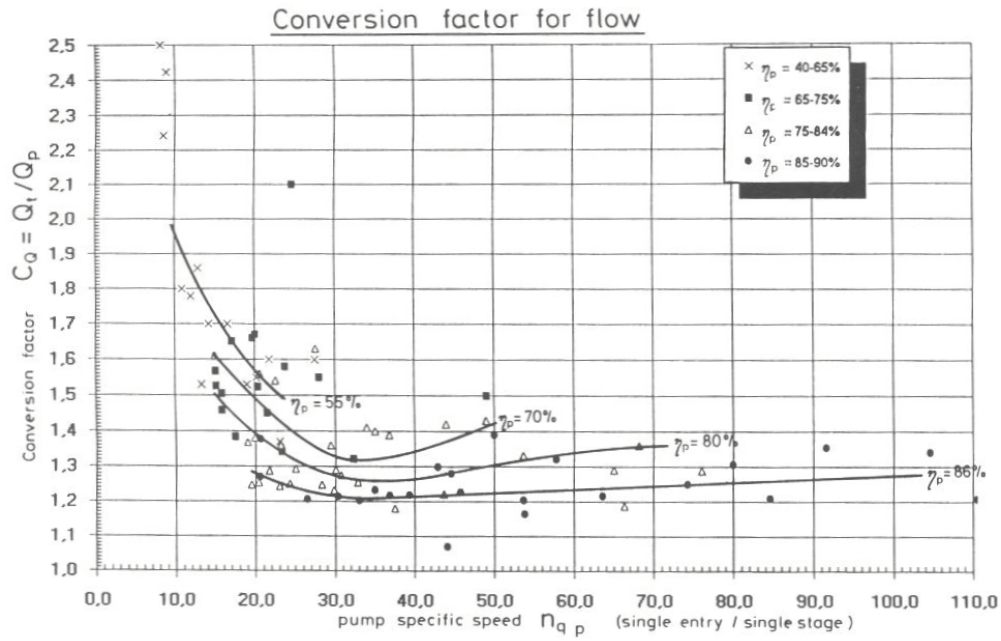


FIGURE D2 :

Factors for the conversion of pump design conditions into turbine design conditions

Figure 21: Curves to determine the flow rate at the BEP [4]

5.5. DETERMINATION OF THE PAT EFFICIENCY

Once the flow rate at the BEP has been calculated, the determination of H with the help of the curve predicted (H - Q) is easy, then the global efficiency can be calculated with equations 56 and 57.

$$\eta_{global\ BEP} = \eta_{hyd\ BEP} \eta_{vol} \eta_{mec} \quad \text{Eq. 56}$$

with

$$\eta_{hyd\ BEP} = \frac{H_{th\ BEP}}{H_{BEP}} \quad \text{Eq. 57}$$

The volumetric efficiency η_{vol} which is almost constant for all flow rates is calculated by the macro Excel with the Equation 51. The mechanical efficiency η_{mec} can be approximated by 0.98.

5.6 RESULTS IN TURBINE OPERATION

5.6.1 Volumetric efficiency

Figure 22 shows the results of the volumetric efficiency modeling according to section 5.1.2. It is observed that the volumetric efficiencies vary between 0.9 and 1 and that the values are quite constant in function of the flow rate. The pump No5 has stepped gaps, which is the reason of lower flow leakages and thus higher volumetric efficiency.

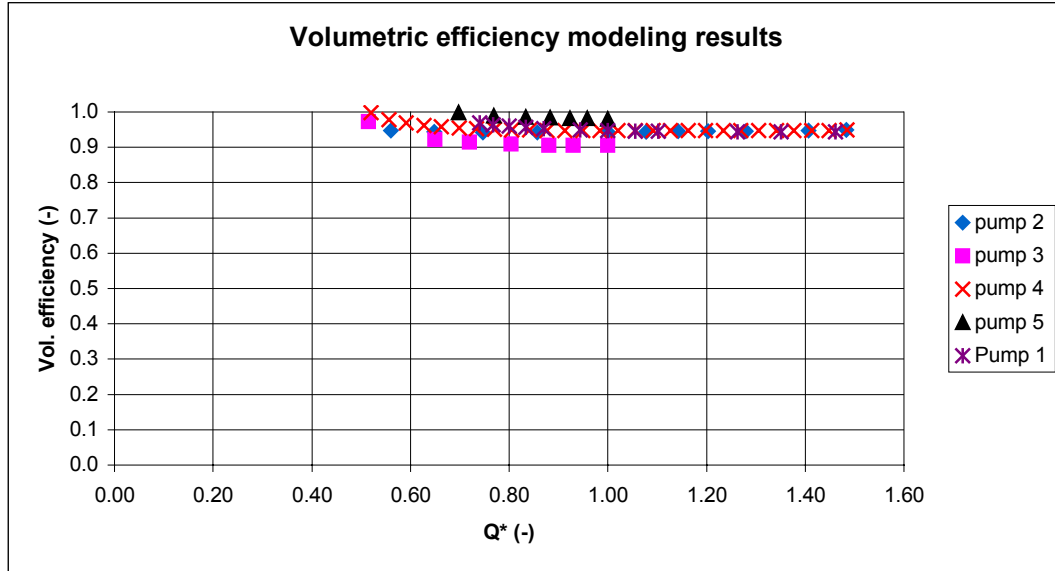


Figure 22: Volumetric efficiency in turbine operation

5.6.2 Theoretical turbine characteristic

The theoretical head curves (H_{th}) obtained with the relations of section 5.1 (Eq. 43) can be seen in Figures 23 to 27. The results are consistent and the zone between the curves represents the losses depending on Q^2 plus the incidence losses which have not been modelised in this project.

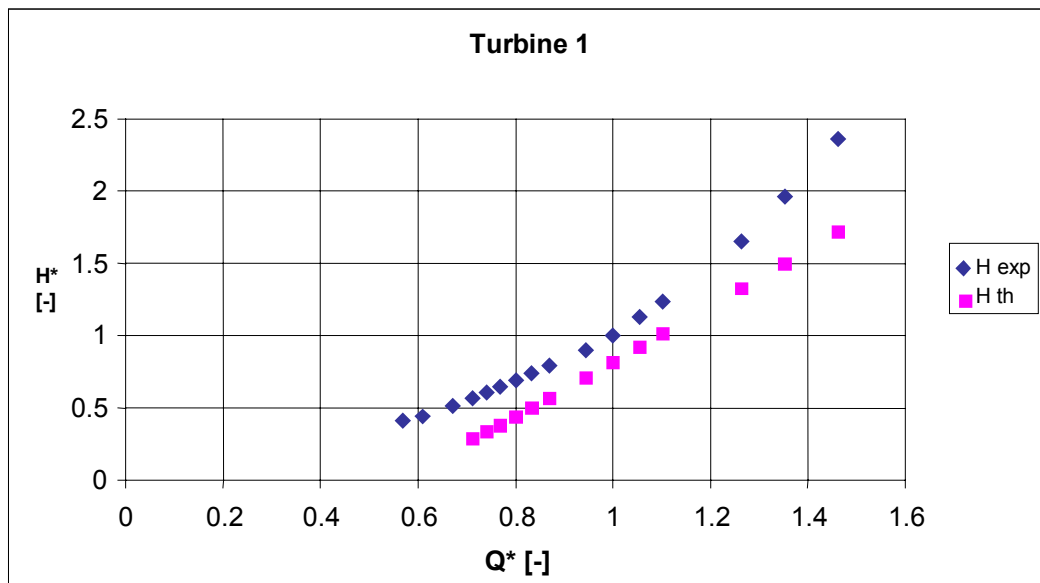


Figure 23: Theoretical characteristic turbine Hth of Pump 1 operating as turbine

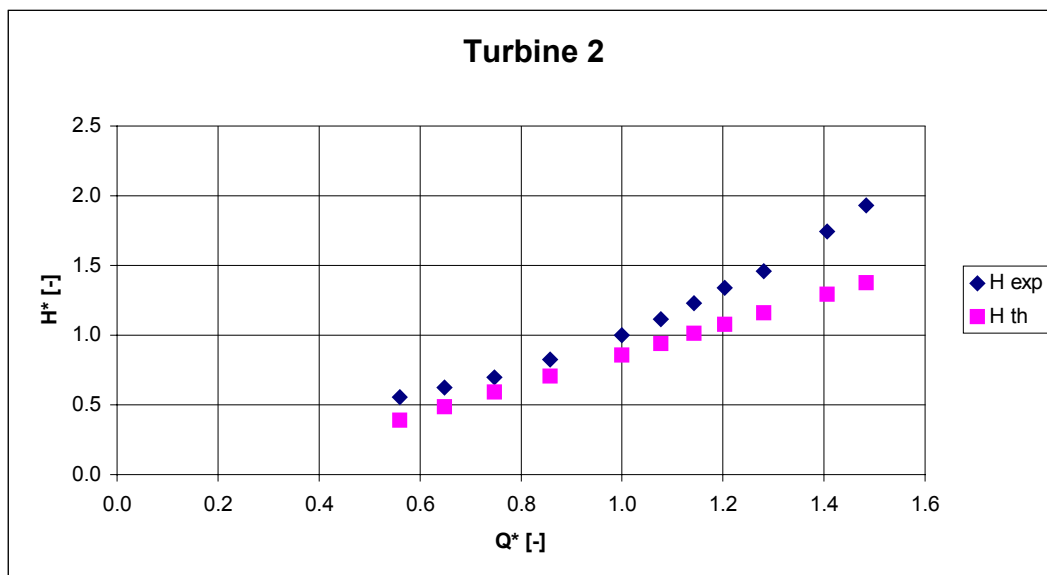


Figure 24: Theoretical characteristic turbine Hth of pump 2 operating as turbine

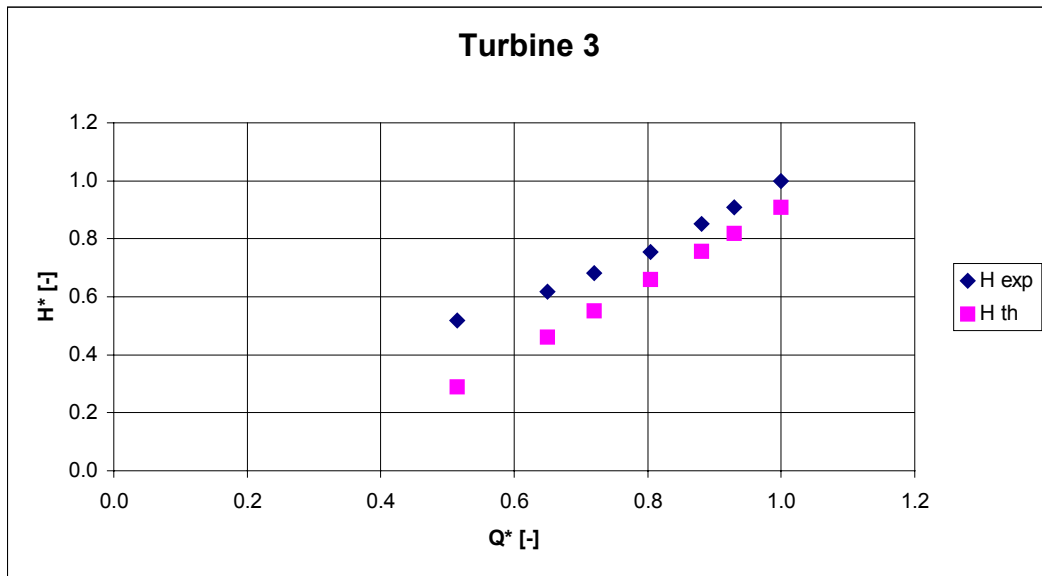


Figure 25: Theoretical characteristic turbine Hth of PUMP 3 operating as turbine

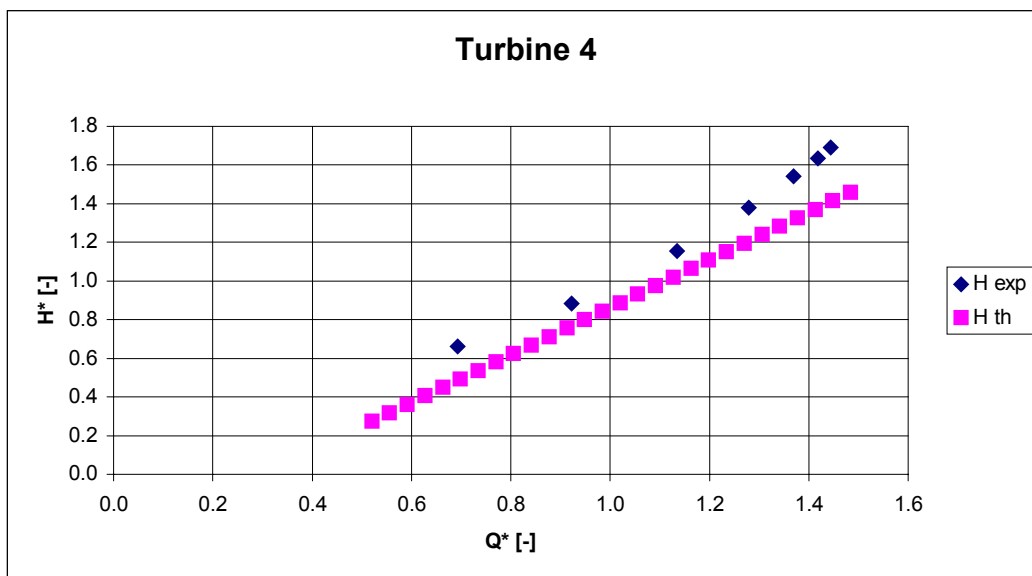


Figure 26: Theoretical characteristic turbine Hth of pump 4 operating as turbine

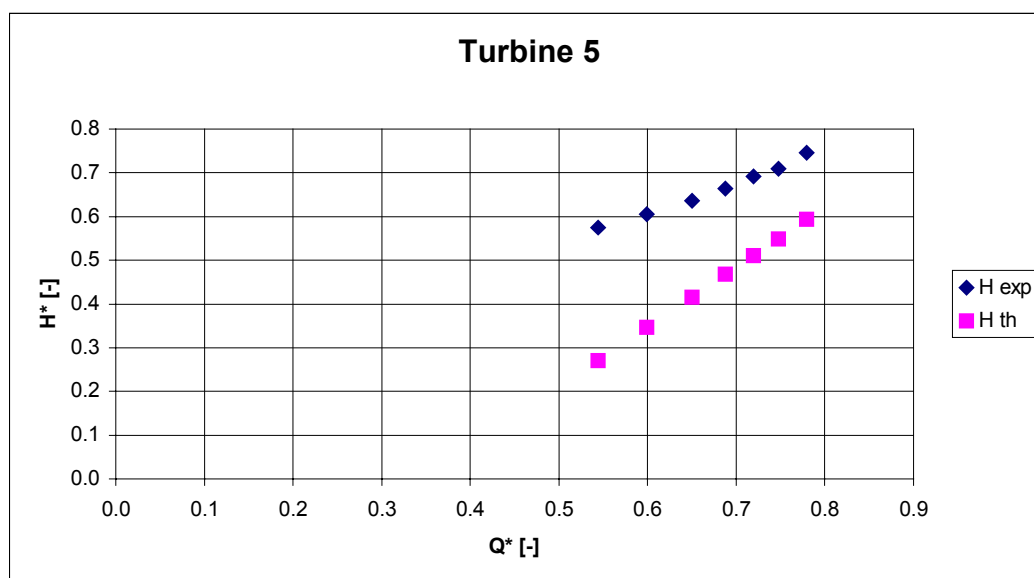


Figure 27: Theoretical characteristic turbine Hth of pump 5 operating as turbine

5.6.3 Prediction

Figures 28 to 32 show the experimental turbine characteristics, the predicted curves and the modeled hydraulic head losses of the pumps studied. Table 3 shows the relative errors between the prediction and the experimental data.

By applying the same model of head losses used for pumps, it was observed that head losses are overestimated in turbine mode (about 10%). In order to match the experimental and the prediction results, at least at the BEP, a factor, which would be applied for any pumps, can be used to decrease the head losses values. With a value of 0.9 for this factor, the head predicted in turbine mode fit the experimental head curve at the BEP with deviations going from 0.4% to 4.6%.

Experimental results for pump No 5 are quite particular; indeed it was observed in the experimental results for others pumps that flow rate at BEP in turbine mode is higher than the flow rate at BEP in pump mode (about 1.3 higher). The experimental results in turbine mode for that pump provided by Sulzer show a flow rate in turbine mode which is smaller than in pump mode. Figure 30 shows the trend of the experimental head curve and the trend of the predicted head. It is observed that the curves join very well at a point which corresponds to the BEP flow rate calculated by the Chapallaz method [4].

Turbine	H* predicted (-)	Relative error on H (%)	Relative error on the efficiency (%)

No 2	1.004	0.37	
No 3	1.045	4.5	
No 4	1.0022	0.22	3
No 5	1.01	1	

Table 3: Relative error between the prediction and the measurement in turbine mod

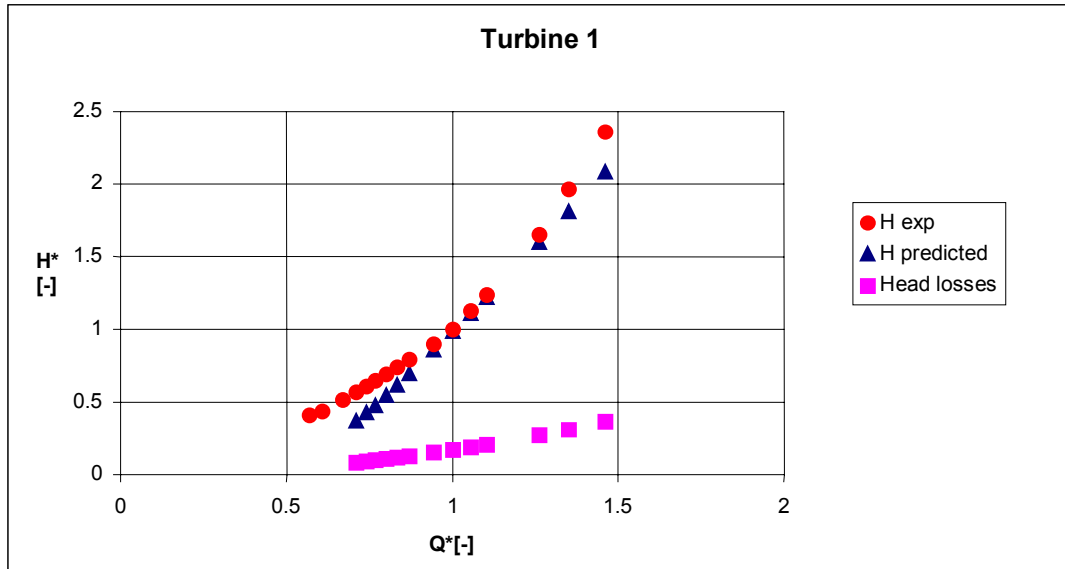


Figure 28: Modeled turbine characteristics and head losses for Pump 1

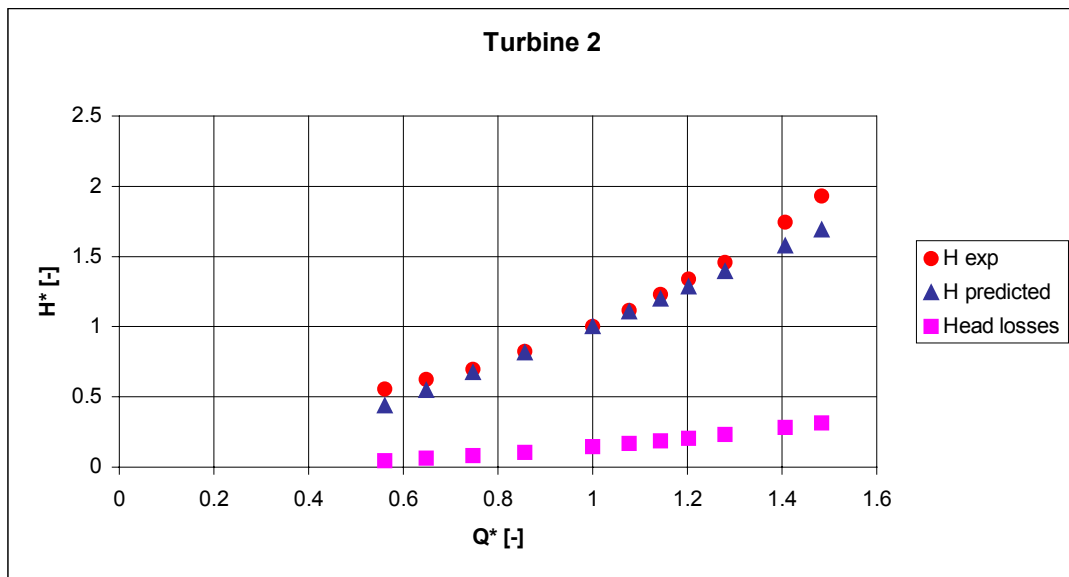


Figure 29: Modeled turbine characteristics and head losses for Pump 2

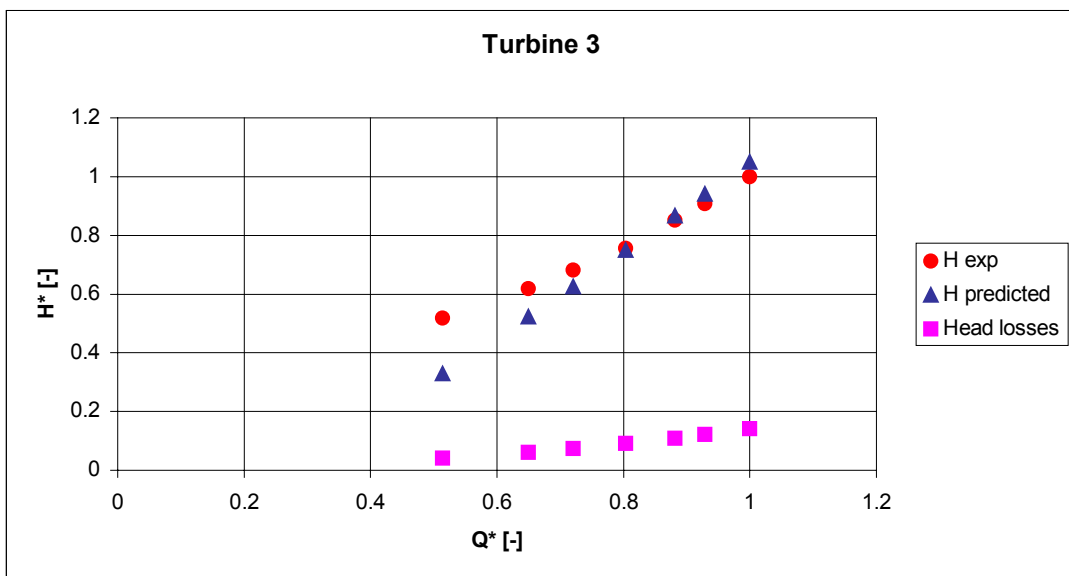


Figure 30: Modeled turbine characteristics and head losses for Pump 3

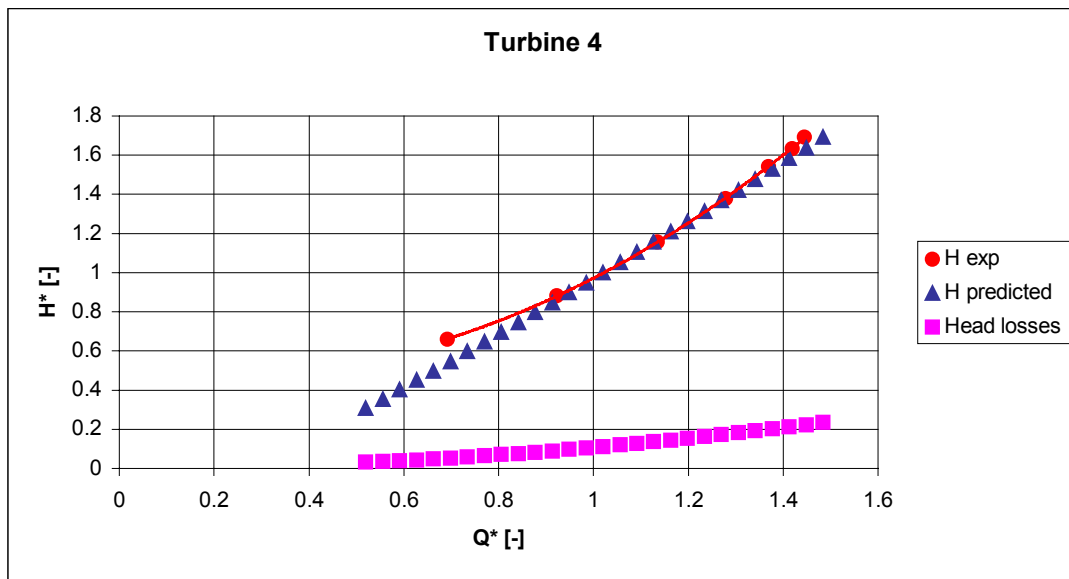


Figure 31: Modeled turbine characteristics and head losses for Pump 4

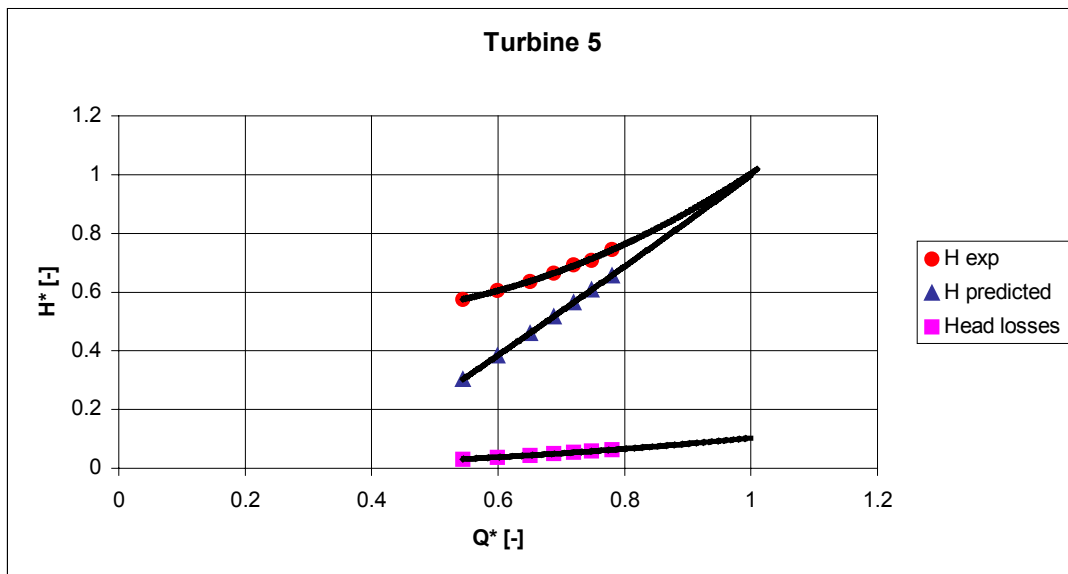


Figure 32: Modeled turbine characteristics and head losses for Pump 5

6. EXPLOITATION DU MOTEUR SYNCHROME EN VITESSE VARIABLE

A la *Haute Ecole Valaisanne (HEVs)*, une installation de laboratoire a été réalisée; elle comprend **une machine synchrone à aimants permanents et un convertisseur de fréquence** développé à la *HEVs*. L'objectif des essais avec 2kW de puissance était de tester différents **algorithmes de réglage** du système à vitesse variable pour la partie onduleur/redresseur du côté réseau et du côté machine (voir Figure 33).

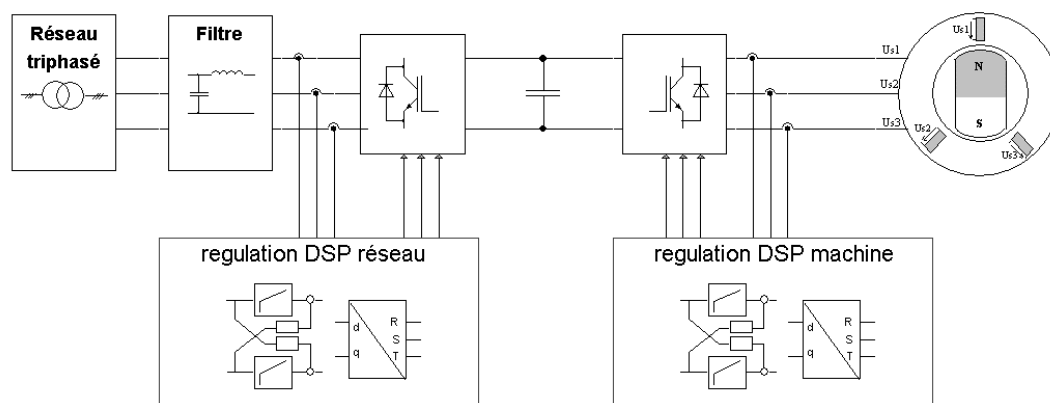


Figure 33 : Schéma bloc du système d'entraînement comprenant un convertisseur de fréquence 4 quadrants et une machine synchrone à aimants permanents

Les algorithmes de régulation se basent sur la théorie du réglage vectoriel. Ils étaient implémentés dans un système à processeur de signal DSP. La régulation de vitesse s'effectue sans capteur de vitesse. La fréquence de commutation des transistors IGBT était choisie à 20kHz pour diminuer les dimensions du filtre du côté réseau. Le système montre un bon rendement en charge partielle (rendement maximal : onduleur 94%, machine 90%, voir Figure 34), avec courants sinusoïdaux et facteur de puissance 1.

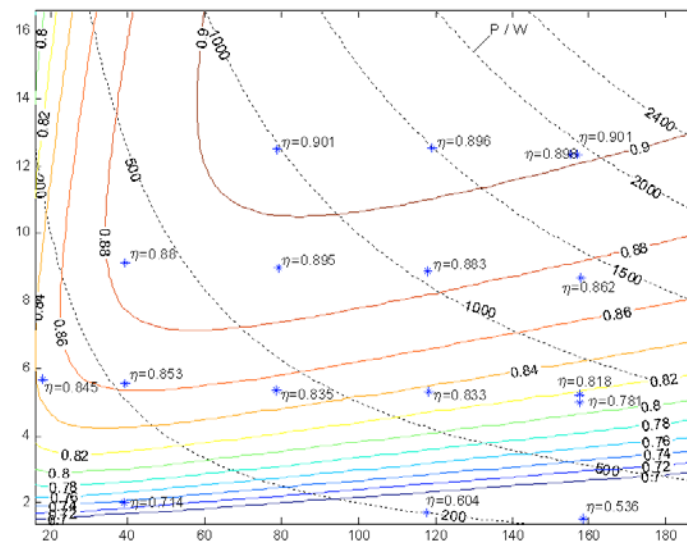


Figure 34 : Diagramme du rendement en fonction du couple M [Nm] et de la vitesse angulaire ω [rad/s]

7. CONCLUSIONS

Le modèle de pertes hydrauliques proposé pour la prédiction de la caractéristique de fonctionnement en turbine d'une pompe, a fourni des résultats très concluants.

Le modèle de pertes a tout d'abord permis de prédire la hauteur de refoulement en pompe au point de meilleur rendement avec une erreur de 4 à 5% par rapport aux mesures.

Le même modèle de pertes appliqué au fonctionnement en turbine nous permet de prédire la chute au point de meilleur rendement avec un écart de 2 à 5 %. Une légère surestimation des pertes hydrauliques en turbine (de l'ordre de 10%) a été trouvée. Ceci mène à introduire un facteur de correction qui est commun pour toutes les machines testées.

Un logiciel programmé sur une feuille EXCEL a été finalisé et elle accompagne ce rapport pour la mis à disposition pour libre utilisation des constructeurs de pompes et des utilisateurs.

Sulzer Pumps, partenaire du projet, est très satisfait des résultats obtenus. De même pour les Services Industriels de Genève qui vont appliquer le logiciel proposé pour qualifier les PATs qu'ils vont acquérir pour la récupération d'énergie dans le retour d'un circuit alimentant des utilisateurs de pompes à chaleur.

Par rapport à l'étude de la génératrice synchrone effectuée à l'HEVS, les résultats obtenus en 2004 ont été valorisés par la publication d'un article, voir référence ci-dessous. Rappelons que, à la suite d'un projet précédent, une pompe Sulzer fonctionnant en turbine à vitesse variable et utilisant une électronique de puissance développée à Sion a été installée sur l'eau potable de la Ville de Sion en 1995. Grâce à la présente étude, l'électronique ainsi que les algorithmes de réglage ont pu être améliorés et adaptés aux derniers développements de l'électronique.

7.1 Travaux publiés dans le cadre du projet

Biner H.-P., Dubas M., Germanier A.: "Small variable speed power plant on a drinking water network", in Proc. European Conference on Power Electronics, Intelligent Motion and Power Quality PCIM, pp. 420-424, Nuremberg 2005.

Danssmann E. : Pompe fonctionnant en turbine. Détermination d'un modèle de pertes pour une pompe et validation pour le fonctionnement en turbine. Travail de diplôme 2004. Ecole d'ingénieurs de Genève.

7.2 Collaboration nationale

Les partenaires du projet sont:

- Sulzer Pumps à Winterthur : Philippe Dupont
- Ecole d'ingénieurs de Genève : Jean Prénat, Jorge Arpe
- Haute Ecole Valaisanne : Michel Dubas, Hans-Peter Biner

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Appendix

A.1 THE VBA EXCEL MACRO

```

Const Pi As Double = 3.141593
Const g As Double = 9.81
Const Rho As Double = 998.23
Const k2 As Double = 3.2
Const epsilon_Q As Double = 0.000001
Const epsilon_vol As Double = 0.0000001

Dim Viscosity As Double

Sub Turbine_operation_DoubleVolute()

Dim Q() As Double, QLa() As Double, QLaz() As Double
Dim cLaz() As Double, Re_La() As Double, HBendLoc_DO() As Double, HBend_Frict_DO() As Double, Hv_DO() As Double, K_DO() As Double
Dim HBendLoc_OSK() As Double, HBend_Frict_OSK() As Double, Hv_OSK() As Double, K_OSK() As Double
Dim HBendLoc_OSDK() As Double, HBend_Frict_OSDK() As Double, Hv_OSDK() As Double, K_OSDK() As Double
Dim zetaSP_outer() As Double, Hv_SP_outer() As Double, K_SP_outer() As Double
Dim HBendLoc_DI() As Double, HBend_Frict_DI() As Double, Hv_DI() As Double, K_DI() As Double
Dim zetaSP_inner() As Double, Hv_SP_inner() As Double, K_SP_inner() As Double
Dim Hv_OuterLeg() As Double, Hv_InnerLeg() As Double, TotalVoluteLosses() As Double, TotalLosses() As Double, HeadPredicted() As Double
Dim K_inner_leg() As Double, K_outer_leg() As Double
Dim c_exit_outer_spiral() As Double, c_exit_inner_spiral() As Double
Dim c_inlet_outer_spiral() As Double
Dim c_inlet_inner_spiral() As Double, Discriminant() As Double, Racine1() As Double, Racine2() As Double
Dim f_Qinner() As Double, df_dQinner() As Double
Dim Q_outer() As Double, Q_inner() As Double, Q_inner_new() As Double
Dim c3q() As Double, c3u() As Double
Dim c2u() As Double, c2m() As Double, TangAlpha2() As Double
Dim beta2() As Double, c1m() As Double
Dim Hth() As Double
Dim Hp() As Double, DeltaHsp() As Double
Dim dsp() As Double, Lsp() As Double, s() As Double
Dim cax0() As Double, LambdaVar0() As Double, LambdaVar1() As Double, cax1() As Double
Dim Tempo() As Double, Qsp() As Double, VolumetricEffic() As Double, Re() As Double
Dim Qexp() As Double, Hexp() As Double, GlobalEffic() As Double
Dim Lambda() As Double
Dim zFrictionBend() As Double, zTotalBend() As Double, kLocalBend() As Double, kFrictionBend() As Double

```

```

Dim kTotalBend() As Double
Dim RunnerHeadLosses() As Double, BendLosses() As Double, FrictionLosses() As Double
Dim SuddenContrLosses2_1() As Double, SuddenContrLosses2_2() As Double, SuddenExpaLosses1() As Double
Dim TotalSuddenLosses() As Double
Dim HydEff() As Double, Hth_exp() As Double, Hth_new() As Double
Dim Graph As ChartObject

'Clear values in the worksheets
Worksheets("RunnerLosses").Range("A:BZ").ClearContents
Worksheets("CasingLosses").Range("A:BZ").ClearContents
Worksheets("Hth-Q").Range("A:BZ").ClearContents
Worksheets("SuddenLosses").Range("A:BZ").ClearContents
Worksheets("VolumetricLosses").Range("A:BZ").ClearContents
Worksheets("TotalLosses").Range("A:BZ").ClearContents

'Clear Graphics in worksheets
Worksheets("RunnerLosses").ChartObjects.Delete
Worksheets("SuddenLosses").ChartObjects.Delete
Worksheets("VolumetricLosses").ChartObjects.Delete
Worksheets("Hth-Q").ChartObjects.Delete
Worksheets("CasingLosses").ChartObjects.Delete
Worksheets("TotalLosses").ChartObjects.Delete

Viscosity = Worksheets("GeneralData").Range("B14").Value
VolumetricEff = Worksheets("GeneralData").Range("B10").Value
MecanichEff = Worksheets("GeneralData").Range("B11").Value
RoughnessRunner = Worksheets("GeneralData").Range("B19").Value
RoughnessVolute = Worksheets("GeneralData").Range("B20").Value
zLa = Worksheets("RunnerGeometry").Range("C3").Value

*****
' Initializing Q, QLa and QLaz
*****

Qmin = Worksheets("GeneralData").Range("B6").Value
Qmax = Worksheets("GeneralData").Range("B7").Value
Qstep = Worksheets("GeneralData").Range("B8").Value
NoPoints = Round(((Qmax - Qmin) / Qstep), 0) + 1

ReDim Q(1 To NoPoints), QLa(1 To NoPoints), QLaz(1 To NoPoints)

Q(1) = Qmin
QLa(1) = Q(1) * VolumetricEff
QLaz(1) = Q(1) * VolumetricEff / zLa

For i = 2 To NoPoints

    Q(i) = Q(i - 1) + Qstep
    QLa(i) = Q(i) * VolumetricEff
    QLaz(i) = Q(i) * VolumetricEff / zLa

Next i

*****
'Assesment of the theoretical characteristics curves in mode turbine H-Q
*****

ReDim c3q(1 To NoPoints), c3u(1 To NoPoints)
ReDim c2u(1 To NoPoints), c2m(1 To NoPoints), TangAlpha2(1 To NoPoints)
ReDim beta2(1 To NoPoints), c1m(1 To NoPoints), Hth(1 To NoPoints)

'Assesment of cu2

A3q_inner = Worksheets("RunnerGeometry").Range("H11").Value
A3q_outer = Worksheets("RunnerGeometry").Range("H12").Value
A3q_total = A3q_inner + A3q_outer

alpha3B_inner = Worksheets("RunnerGeometry").Range("Q9").Value
alpha3B_outer = Worksheets("RunnerGeometry").Range("Q10").Value
alpha3B_average = (alpha3B_inner + alpha3B_outer) / 2

u1 = Worksheets("RunnerGeometry").Range("K14").Value
u2 = Worksheets("RunnerGeometry").Range("N14").Value

A_1 = Worksheets("RunnerGeometry").Range("K7").Value
A_2 = Worksheets("RunnerGeometry").Range("N7").Value

d2 = Worksheets("RunnerGeometry").Range("E6").Value
d3 = Worksheets("RunnerGeometry").Range("H6").Value

```

```

Beta1 = Worksheets("RunnerGeometry").Range("K10").Value

For i = 1 To NoPoints

    c3q(i) = Q(i) / A3q_total

    c3u(i) = c3q(i) * Cos(alpha3B_average * Pi / 180)
    c2u(i) = (d3 / d2) * c3u(i)

    c2m(i) = QLa(i) / A_2

    TangAlpha2(i) = c2m(i) / c2u(i)

    beta2(i) = Atn(c2m(i) / (u2 - c2u(i))) * 180 / Pi

    c1m(i) = QLa(i) / A_1
    Factor = 0.905
    Hth(i) = (Factor * (u2 * c2m(i) / TangAlpha2(i) + u1 * c1m(i) / Tan(Beta1 * Pi / 180)) - u1 ^ 2) / g

    Worksheets("Hth-Q").Range("A1") = "Q(m3/s)"
    Worksheets("Hth-Q").Range("A" & i + 1) = Q(i)

    Worksheets("Hth-Q").Range("B1") = "beta2(m)"
    Worksheets("Hth-Q").Range("B" & i + 1) = beta2(i)

    Worksheets("Hth-Q").Range("C1") = "Hth(m)"
    Worksheets("Hth-Q").Range("C" & i + 1) = Hth(i)

Next i

' Plotting Hth-Q

Set Graph = Worksheets("Hth-Q").ChartObjects.Add(200, 100, 400, 250)
Graph.Chart.ChartType = xlXYScatter
Graph.Chart.SetSourceData Worksheets("Hth-Q").Range("A:A,C:C")
With Graph.Chart
    .HasTitle = True
    .ChartTitle.Characters.Text = "Hth-Q"
    .Axes(xlCategory, xlPrimary).HasTitle = True
    .Axes(xlCategory, xlPrimary).AxisTitle.Characters.Text = "Q[m^3/s]"
    .Axes(xlValue, xlPrimary).HasTitle = True
    .Axes(xlValue, xlPrimary).AxisTitle.Characters.Text = "H[m]"
End With

*****
' Assesment of the flow leakages and volumetric efficiency
*****

ReDim Hp(1 To NoPoints), DeltaHsp(1 To NoPoints)
ReDim cax0(1 To NoPoints), LambdaVar0(1 To NoPoints), LambdaVar1(1 To NoPoints), cax1(1 To NoPoints)
ReDim Tempo(1 To NoPoints), Qsp(1 To NoPoints), VolumetricEffic(1 To NoPoints), Re(1 To NoPoints)

u2 = Worksheets("RunnerGeometry").Range("N14").Value
d2 = Worksheets("RunnerGeometry").Range("E6").Value
k = Worksheets("GapData").Range("H5").Value

' Reading the gap data

NoGaps = Worksheets("GapData").Range("B13").Value
zEA = Worksheets("GapData").Range("B3").Value
zK = Worksheets("GapData").Range("B4").Value
a = Worksheets("GapData").Range("B5").Value
Reu = Worksheets("GapData").Range("H8").Value

ReDim dsp(1 To NoGaps), Lsp(1 To NoGaps), s(1 To NoGaps)

For j = 1 To NoGaps
    dsp(j) = Worksheets("GapData").Cells(9, j + 1)
    s(j) = Worksheets("GapData").Cells(10, j + 1)
    Lsp(j) = Worksheets("GapData").Cells(11, j + 1)
Next j

'Computing DeltaHsp, the pressure difference along the gap

For i = 1 To NoPoints
    Hp(i) = 0.75 * Hth(i)
    DeltaHsp(i) = Hp(i) - ((k ^ 2 * u2 ^ 2) / (2 * g)) * (1 - dsp(1) ^ 2 / d2 ^ 2)
    Worksheets("VolumetricLosses").Range("B1") = "DeltaHsp(m)"
    Worksheets("VolumetricLosses").Range("B" & i + 1) = DeltaHsp(i)
Next i

'Computing Cax, axial speed trough the gap, iteratif computation

```



```

LambdaVar = 0

If NoGaps = 1 Then
    Factor = 0
Else
    Factor = 1
    Temp = 0
    For i = 2 To NoGaps
        V = (dsp(1) / dsp(i)) ^ 2 * (s(1) / s(i)) ^ 2 * (zK + 0.5 * LambdaVar * Lsp(i) / s(i)) + Temp
        Temp = V
    Next i
End If

For i = 1 To NoPoints
    cax0(i) = ((2 * g * DeltaHsp(i)) / (zEA + (LambdaVar * Lsp(1)) / (2 * s(1)) + Factor * V)) ^ 0.5
Next i

Tempo = cax0

Do
    For i = 1 To NoPoints
        Re(i) = 2 * s(1) * Tempo(i) / Viscosity
        LambdaVar0(i) = 0.31 / (Log10(a + 6.5 / Re(i))) ^ 2
        LambdaVar1(i) = LambdaVar0(i) * (1 + 0.19 * (Reu / Re(i)) ^ 2) ^ 0.375

        If NoGaps = 1 Then
            Factor = 0
        Else
            Factor = 1
            Temp = 0
            For k = 2 To NoGaps
                V = (dsp(1) / dsp(k)) ^ 2 * (s(1) / s(k)) ^ 2 * (zK + 0.5 * LambdaVar1(i) * Lsp(k) / s(k)) + Temp
                Temp = V
            Next k
        End If

        cax1(i) = Sqr((2 * g * DeltaHsp(i)) / (zEA + (LambdaVar1(i) * Lsp(1)) / (2 * s(1)) + Factor * V))
    Next i

    j = 1
    Do
        If Abs((cax1(j) - Tempo(j))) > epsilon_vol Then
            Tempo = cax1
            Flag = 0
        Else
            j = j + 1
            Flag = 1
        End If
    Loop While Flag = 1 And j < NoPoints
Loop While Flag = 0

'Computing the volumetric efficiency

For i = 1 To NoPoints
    Qsp(i) = Pi * dsp(1) * s(1) * cax1(i)
    VolumetricEffic(i) = (Q(i) - Qsp(i)) / Q(i)

    Worksheets("VolumetricLosses").Range("A1") = "Q(m/s)"
    Worksheets("VolumetricLosses").Range("A" & i + 1) = Q(i)
    Worksheets("VolumetricLosses").Range("C1") = "Lambda(m/s)"
    Worksheets("VolumetricLosses").Range("C" & i + 1) = LambdaVar1(i)
    Worksheets("VolumetricLosses").Range("D1") = "Cax(m/s)"
    Worksheets("VolumetricLosses").Range("D" & i + 1) = cax1(i)
    Worksheets("VolumetricLosses").Range("E1") = "Qsp(m3/s)"
    Worksheets("VolumetricLosses").Range("E" & i + 1) = Qsp(i)
    Worksheets("VolumetricLosses").Range("F1") = "Vol.Efficiency(-)"
    Worksheets("VolumetricLosses").Range("F" & i + 1) = VolumetricEffic(i)
Next i

' Plotting the Volumetric Efficiency vs Q

Set Graph = Worksheets("VolumetricLosses").ChartObjects.Add(400, 120, 400, 250)
Graph.Chart.ChartType = xlXYScatter
Graph.Chart.SetSourceData Worksheets("VolumetricLosses").Range("A:A,F:F")
With Graph.Chart

```

```

.HasTitle = True
.ChartTitle.Characters.Text = "Assesment of the Volumetric Efficiency"
.Axes(xlCategory, xlPrimary).HasTitle = True
.Axes(xlCategory, xlPrimary).AxisTitle.Characters.Text = "Q(m3/s)"
.Axes(xlValue, xlPrimary).HasTitle = True
.Axes(xlValue, xlPrimary).AxisTitle.Characters.Text = "Volumetric Efficiency[-]"
.Axes(xlValue).MinimumScale = 0
.Axes(xlValue).MaximumScale = 1
End With

*****
'Computation of the QLa and QLza taking account the volumetric losses calculated above
*****
For i = 1 To NoPoints

    QLa(i) = Q(i) * VolumetricEffic(i)
    QLaz(i) = Q(i) * VolumetricEffic(i) / zLa

Next i

*****
'Assesment of the losses in the volute: determination of the flow rate in each leg
*****
ReDim Q_outer(1 To NoPoints), Q_inner(1 To NoPoints), Q_inner_new(1 To NoPoints)

ReDim HBendLoc_DO(1 To NoPoints), HBend_Frict_DO(1 To NoPoints), Hv_DO(1 To NoPoints), K_DO(1 To NoPoints)
ReDim HBendLoc_OSK(1 To NoPoints), HBend_Frict_OSK(1 To NoPoints), Hv_OSK(1 To NoPoints), K_OSK(1 To NoPoints)
ReDim HBendLoc OSDK(1 To NoPoints), HBend_Frict OSDK(1 To NoPoints), Hv OSDK(1 To NoPoints), K OSDK(1 To NoPoints)
ReDim zetaSP_outer(1 To NoPoints), Hv_SP_outer(1 To NoPoints), K_SP_outer(1 To NoPoints)
ReDim c_exit_outer_spiral(1 To NoPoints), c_inlet_outer_spiral(1 To NoPoints)

ReDim HBendLoc_DI(1 To NoPoints), HBend_Frict_DI(1 To NoPoints), Hv_DI(1 To NoPoints), K_DI(1 To NoPoints)
ReDim zetaSP_inner(1 To NoPoints), Hv_SP_inner(1 To NoPoints), K_SP_inner(1 To NoPoints)
ReDim c_exit_inner_spiral(1 To NoPoints), c_inlet_inner_spiral(1 To NoPoints)

ReDim Hv_OuterLeg(1 To NoPoints), Hv_InnerLeg(1 To NoPoints), TotalVoluteLosses(1 To NoPoints), TotalLosses(1 To NoPoints)
ReDim HeadPredicted(1 To NoPoints)
ReDim f_Qinner(1 To NoPoints), df_dQinner(1 To NoPoints)
ReDim K_inner_leg(1 To NoPoints), K_outer_leg(1 To NoPoints), Discriminant(1 To NoPoints), Racine1(1 To NoPoints), Racine2(1 To NoPoints)

'Initialization of the flow rates in each leg

TotalAngle_inner_spiral = Worksheets("RunnerGeometry").Range("H13").Value
TotalAngle_outer_spiral = Worksheets("RunnerGeometry").Range("H14").Value

For i = 1 To NoPoints

    Q_inner(i) = (150 / 360) * Q(i)
    Q_outer(i) = Q(i) - Q_inner(i)

    Worksheets("CasingLosses").Range("B1") = "Q_outer_init(m3/s)"
    Worksheets("CasingLosses").Range("B" & i + 1) = Q_outer(i)
    Worksheets("CasingLosses").Range("C1") = "Q_inner_init(m3/s)"
    Worksheets("CasingLosses").Range("C" & i + 1) = Q_inner(i)

Next i

'Iteratif loop to determine flowrate through each leg
Do

    For i = 1 To NoPoints

        j = 4
        Q_outer(i) = Q(i) - Q_inner(i)

        'Losses in the outer discharge

        TempHBendLocal = 0
        TempHBendFric = 0

        If Worksheets("CasingGeometry").Range("B" & j) = "OuterDisch" Then

            Ain_outer_leg = Worksheets("CasingGeometry").Range("H" & j).Value

            Do
                Dhin = Worksheets("CasingGeometry").Range("O" & j).Value
                Dhout = Worksheets("CasingGeometry").Range("P" & j).Value
                Lm = Worksheets("CasingGeometry").Range("M" & j).Value
            
```

```

Angle = Worksheets("CasingGeometry").Range("C" & j).Value
Ro = Worksheets("CasingGeometry").Range("L" & j).Value
Dh = 0.5 * (Dhin + Dhout)
Aref = (Pi / 4) * Dh ^ 2
c_ref_DO = Q_outer(i) / Aref

zBendLocal_DO = BendLocal(Angle, Ro, Dh)
HBendLocal_DO = (zBendLocal_DO * c_ref_DO ^ 2) / (2 * g) + TempHBendLocal
TempHBendLocal = HBendLocal_DO

Re_DO = Reynolds(c_ref_DO, Dh, Viscosity)
DeltaRelative_DO = RoughnessVolute / Dh
LambdaTube = TubeFrictionCoefficient(Re_DO, DeltaRelative_DO)

zBend_Friction_DO = BendFriction(LambdaTube, Ro, Dh, Angle)
HBend_Friction_DO = (zBend_Friction_DO * c_ref_DO ^ 2) / (2 * g) + TempHBendFric
TempHBendFric = HBend_Friction_DO

j = j + 1

Loop While Worksheets("CasingGeometry").Range("B" & j) = "OuterDisch"

HBendLoc_DO(i) = HBendLocal_DO
HBend_Frict_DO(i) = HBend_Friction_DO

Worksheets("CasingLosses").Range("D1") = "H_Bend_DO(m)"
Worksheets("CasingLosses").Range("D" & i + 1) = HBendLoc_DO(i)
Worksheets("CasingLosses").Range("E1") = "H_BendFr_DO(m)"
Worksheets("CasingLosses").Range("E" & i + 1) = HBend_Frict_DO(i)

Hv_DO(i) = HBendLoc_DO(i) + HBend_Frict_DO(i)
K_DO(i) = (g * Hv_DO(i)) / Q_outer(i) ^ 2

Worksheets("CasingLosses").Range("F1") = "Hv_DO(m)"
Worksheets("CasingLosses").Range("F" & i + 1) = Hv_DO(i)
Worksheets("CasingLosses").Range("G1") = "K_DO"
Worksheets("CasingLosses").Range("G" & i + 1) = K_DO(i)

End If

'Losses in the outer channel

TempHBendLocal = 0
TempHBendFric = 0

If Worksheets("CasingGeometry").Range("B" & j) = "OSK" Then

Do
Dhin = Worksheets("CasingGeometry").Range("O" & j).Value
Dhout = Worksheets("CasingGeometry").Range("P" & j).Value
Lm = Worksheets("CasingGeometry").Range("M" & j).Value

Angle = Worksheets("CasingGeometry").Range("C" & j).Value
Ro = Worksheets("CasingGeometry").Range("L" & j).Value
Dh = 0.5 * (Dhin + Dhout)
Aref = (Pi / 4) * Dh ^ 2
c_ref_OSK = Q_outer(i) / Aref

zBendLocal_OSK = BendLocal(Angle, Ro, Dh)

HBendLocal_OSK = (zBendLocal_OSK * c_ref_OSK ^ 2) / (2 * g) + TempHBendLocal
TempHBendLocal = HBendLocal_OSK

Re_OSK = Reynolds(c_ref_OSK, Dh, Viscosity)
DeltaRelative_OSK = RoughnessVolute / Dh
LambdaTube = TubeFrictionCoefficient(Re_OSK, DeltaRelative_OSK)

zBend_Friction_OSK = BendFriction(LambdaTube, Ro, Dh, Angle)
HBend_Friction_OSK = (zBend_Friction_OSK * c_ref_OSK ^ 2) / (2 * g) + TempHBendFric
TempHBendFric = HBend_Friction_OSK

j = j + 1

Loop While Worksheets("CasingGeometry").Range("B" & j) = "OSK"

HBendLoc_OSK(i) = HBendLocal_OSK
HBend_Frict_OSK(i) = HBend_Friction_OSK

Worksheets("CasingLosses").Range("H1") = "H_Bend_OSK(m)"
Worksheets("CasingLosses").Range("H" & i + 1) = HBendLoc_OSK(i)
Worksheets("CasingLosses").Range("I1") = "H_BendFr_OSK(m)"

```

```

Worksheets("CasingLosses").Range("I" & i + 1) = HBend_Frict_OSK(i)

Hv_OSK(i) = HBendLoc_OSK(i) + HBend_Frict_OSK(i)
K_OSK(i) = (g * Hv_OSK(i)) / Q_outer(i) ^ 2

Worksheets("CasingLosses").Range("J1") = "Hv_OSK(m)"
Worksheets("CasingLosses").Range("J" & i + 1) = Hv_OSK(i)
Worksheets("CasingLosses").Range("K1") = "K_OSK"
Worksheets("CasingLosses").Range("K" & i + 1) = K_OSK(i)

End If

'Losses in the outer diffuser channel

TempHBendLocal = 0
TempHBendFric = 0

If Worksheets("CasingGeometry").Range("B" & j) = "OSDK" Then

Do
    Dhin = Worksheets("CasingGeometry").Range("O" & j).Value
    Dhout = Worksheets("CasingGeometry").Range("P" & j).Value
    Lm = Worksheets("CasingGeometry").Range("M" & j).Value

    Angle = Worksheets("CasingGeometry").Range("C" & j).Value
    Ro = Worksheets("CasingGeometry").Range("L" & j).Value
    Dh = 0.5 * (Dhin + Dhout)
    Aref = (Pi / 4) * Dh ^ 2
    c_ref_OSDK = Q_outer(i) / Aref

    zBendLocal_OSDK = BendLocal(Angle, Ro, Dh)

    HBendLocal_OSDK = (zBendLocal_OSDK * c_ref_OSDK ^ 2) / (2 * g) + TempHBendLocal
    TempHBendLocal = HBendLocal_OSDK

    Re_OSDK = Reynolds(c_ref_OSDK, Dh, Viscosity)
    DeltaRelative_OSDK = RoughnessVolute / Dh
    LambdaTube = TubeFrictionCoefficient(Re_OSDK, DeltaRelative_OSDK)

    zBend_Friction_OSDK = BendFriction(LambdaTube, Ro, Dh, Angle)
    HBend_Friction_OSDK = (zBend_Friction_OSDK * c_ref_OSDK ^ 2) / (2 * g) + TempHBendFric
    TempHBendFric = HBend_Friction_OSDK

    j = j + 1

Loop While Worksheets("CasingGeometry").Range("B" & j) = "OSDK"

Aout_outer_leg = Worksheets("CasingGeometry").Range("J" & j - 1).Value

HBendLoc_OSDK(i) = HBendLocal_OSDK
HBend_Frict_OSDK(i) = HBend_Friction_OSDK

Worksheets("CasingLosses").Range("L1") = "H_Bend_OSDK(m)"
Worksheets("CasingLosses").Range("L" & i + 1) = HBendLoc_OSDK(i)
Worksheets("CasingLosses").Range("M1") = "H_BendFr_OSDK(m)"
Worksheets("CasingLosses").Range("M" & i + 1) = HBend_Frict_OSDK(i)

Hv_OSDK(i) = HBendLoc_OSDK(i) + HBend_Frict_OSDK(i)
K_OSDK(i) = g * Hv_OSDK(i) / Q_outer(i) ^ 2

Worksheets("CasingLosses").Range("N1") = "Hv_OSDK(m)"
Worksheets("CasingLosses").Range("N" & i + 1) = Hv_OSDK(i)
Worksheets("CasingLosses").Range("O1") = "K_OSDK"
Worksheets("CasingLosses").Range("O" & i + 1) = K_OSDK(i)

End If

'Losses in the outer spiral

TempPhi = 0
TempPd = 0

If Worksheets("CasingGeometry").Range("B" & j) = "OuterSpiral" Then

    Aref_SP_outer = Worksheets("CasingGeometry").Range("H" & j).Value

    Do
        phi = Worksheets("CasingGeometry").Range("C" & j).Value + TempPhi
        TempPhi = phi
        Phi2 = TempPhi - Worksheets("CasingGeometry").Range("C" & j).Value

        Q_phi = ((TotalAngle_outer_spiral - Phi2) / TotalAngle_outer_spiral) * Q_outer(i)

```

```

A_phi = Worksheets("CasingGeometry").Range("H" & j).Value
c_phi = Q_phi / A_phi

L_phi = Worksheets("CasingGeometry").Range("M" & j).Value
Re_phi = Reynolds(c_phi, L_phi, Viscosity)

Flat_Rel_Roughness = RoughnessVolute / L_phi
cf_phi = FlatPlateFrictionCoefficient(Re_phi, Flat_Rel_Roughness)

U_phi = Worksheets("CasingGeometry").Range("N" & j).Value
Pd = 0.5 * cf_phi * Rho * c_phi ^ 3 * L_phi * U_phi + TempPd
TempPd = Pd

j = j + 1

Loop While Worksheets("CasingGeometry").Range("B" & j) = "OuterSpiral"

c_ref_SP_outer = Q_outer(i) / Aref_SP_outer

zetaSP_outer(i) = (2 * Pd) / (Rho * Aref_SP_outer * c_ref_SP_outer ^ 3)
Hv_SP_outer(i) = (zetaSP_outer(i) * c_ref_SP_outer ^ 2) / (2 * g)
K_SP_outer(i) = g * Hv_SP_outer(i) / Q_outer(i) ^ 2

Worksheets("CasingLosses").Range("P1") = "zSP_outer(-)"
Worksheets("CasingLosses").Range("P" & i + 1) = zetaSP_outer(i)
Worksheets("CasingLosses").Range("Q1") = "HSP_outer(m)"
Worksheets("CasingLosses").Range("Q" & i + 1) = Hv_SP_outer(i)
Worksheets("CasingLosses").Range("R1") = "K_SP_outer"
Worksheets("CasingLosses").Range("R" & i + 1) = K_SP_outer(i)

End If

'Losses in the inner discharge

TempHBendLocal = 0
TempHBendFric = 0

If Worksheets("CasingGeometry").Range("B" & j) = "InnerDisch" Then

    Ain_inner_leg = Worksheets("CasingGeometry").Range("H" & j).Value

    Do
        Dhin = Worksheets("CasingGeometry").Range("O" & j).Value
        Dhout = Worksheets("CasingGeometry").Range("P" & j).Value
        Lm = Worksheets("CasingGeometry").Range("M" & j).Value

        Angle = Worksheets("CasingGeometry").Range("C" & j).Value
        Ro = Worksheets("CasingGeometry").Range("L" & j).Value
        Dh = 0.5 * (Dhin + Dhout)
        Aref = (Pi / 4) * Dh ^ 2
        c_ref_DI = Q_inner(i) / Aref

        zBendLocal_DI = BendLocal(Angle, Ro, Dh)
        HBendLocal_DI = (zBendLocal_DI * c_ref_DI ^ 2) / (2 * g) + TempHBendLocal
        TempHBendLocal = HBendLocal_DI

        Re_DI = Reynolds(c_ref_DI, Dh, Viscosity)
        DeltaRelative_DI = RoughnessVolute / Dh
        LambdaTube = TubeFrictionCoefficient(Re_DI, DeltaRelative_DI)

        zBend_Friction_DI = BendFriction(LambdaTube, Ro, Dh, Angle)
        HBend_Friction_DI = (zBend_Friction_DI * c_ref_DI ^ 2) / (2 * g) + TempHBendFric
        TempHBendFric = HBend_Friction_DI

    Loop While Worksheets("CasingGeometry").Range("B" & j) = "InnerDisch"

    Aout_inner_leg = Worksheets("CasingGeometry").Range("J" & j - 1).Value

    HBendLoc_DI(i) = HBendLocal_DI
    HBend_Frict_DI(i) = HBend_Friction_DI

    Worksheets("CasingLosses").Range("S1") = "H_Bend_DI(m)"
    Worksheets("CasingLosses").Range("S" & i + 1) = HBendLoc_DI(i)
    Worksheets("CasingLosses").Range("T1") = "H_BendFr_DI(m)"
    Worksheets("CasingLosses").Range("T" & i + 1) = HBend_Frict_DI(i)

    Hv_DI(i) = HBendLoc_DI(i) + HBend_Frict_DI(i)
    K_DI(i) = g * Hv_DI(i) / Q_inner(i) ^ 2

```

```

Worksheets("CasingLosses").Range("U1") = "Hv_DI(m)"
Worksheets("CasingLosses").Range("U" & i + 1) = Hv_DI(i)
Worksheets("CasingLosses").Range("V1") = "K_DI"
Worksheets("CasingLosses").Range("V" & i + 1) = K_DI(i)

End If

'Losses in the inner spiral

TempPhi = 0
TempPd = 0

If Worksheets("CasingGeometry").Range("B" & j) = "InnSpiral" Then

    Aref_SP_inner = Worksheets("CasingGeometry").Range("H" & j).Value

    Do
        phi = Worksheets("CasingGeometry").Range("C" & j).Value + TempPhi
        TempPhi = phi
        Phi2 = TempPhi - Worksheets("CasingGeometry").Range("C" & j).Value

        Q_phi = ((TotalAngle_inner_spiral - Phi2) / TotalAngle_inner_spiral) * Q_inner(i)
        A_phi = Worksheets("CasingGeometry").Range("H" & j).Value
        c_phi = Q_phi / A_phi

        L_phi = Worksheets("CasingGeometry").Range("M" & j).Value
        Re_phi = Reynolds(c_phi, L_phi, Viscosity)

        Flat_Rel_Roughness = RoughnessVolute / L_phi
        cf_phi = FlatPlateFrictionCoefficient(Re_phi, Flat_Rel_Roughness)

        U_phi = Worksheets("CasingGeometry").Range("N" & j).Value
        Pd = 0.5 * cf_phi * Rho * c_phi ^ 3 * L_phi * U_phi + TempPd
        TempPd = Pd

        j = j + 1

    Loop While Worksheets("CasingGeometry").Range("B" & j) = "InnSpiral"

    c_ref_SP_inner = Q_inner(i) / Aref_SP_inner

    zetaSP_inner(i) = (2 * Pd) / (Rho * Aref_SP_inner * c_ref_SP_inner ^ 3)
    Hv_SP_inner(i) = (zetaSP_inner(i) * c_ref_SP_inner ^ 2) / (2 * g)
    K_SP_inner(i) = g * Hv_SP_inner(i) / Q_inner(i) ^ 2

    Worksheets("CasingLosses").Range("W1") = "zSP_inner(-)"
    Worksheets("CasingLosses").Range("W" & i + 1) = zetaSP_inner(i)
    Worksheets("CasingLosses").Range("X1") = "HSP_inner(m)"
    Worksheets("CasingLosses").Range("X" & i + 1) = Hv_SP_inner(i)
    Worksheets("CasingLosses").Range("Y1") = "K_SP_inner"
    Worksheets("CasingLosses").Range("Y" & i + 1) = K_SP_inner(i)

End If

'mean velocity at the inlet of the outer channel
c_inlet_outer_spiral(i) = Q_outer(i) / Ain_outer_leg

'mean velocity at the exit of the outer channel (portour of the outer spiral)

L = ((Worksheets("RunnerGeometry").Range("H6").Value) / 2) * (TotalAngle_outer_spiral * Pi / 180) 'd3/2*angle
B3 = Worksheets("RunnerGeometry").Range("H7").Value
A_exit_outer_spiral = L * B3
c_exit_outer_spiral(i) = Q_outer(i) / A_exit_outer_spiral

'mean velocity at the inlet of the inner channel
c_inlet_inner_spiral(i) = Q_inner(i) / Ain_inner_leg

'mean velocity at the exit of the inner channel (portour of the inner spiral)

L = ((Worksheets("RunnerGeometry").Range("H6").Value) / 2) * (TotalAngle_inner_spiral * Pi / 180) 'd3/2*angle
A_exit_inner_spiral = L * B3
c_exit_inner_spiral(i) = Q_inner(i) / A_exit_inner_spiral

'Factor K of the head losses in the volute (gH=KQ^2)

Hv_OuterLeg(i) = Hv_DO(i) + Hv_OSK(i) + Hv_OSDK(i) + Hv_SP_outer(i)
Hv_InnerLeg(i) = Hv_DI(i) + Hv_SP_inner(i)
TotalVoluteLosses(i) = 0.5 * (Hv_OuterLeg(i) + Hv_InnerLeg(i))

K_inner_leg(i) = Hv_InnerLeg(i) * g / Q_inner(i) ^ 2
K_outer_leg(i) = Hv_OuterLeg(i) * g / Q_outer(i) ^ 2

```

' Second degree Function to solve

$$f_Qinner(i) = K_inner_leg(i) * Q_inner(i) ^ 2 - K_outer_leg(i) * (Q(i) - Q_inner(i)) ^ 2$$

'Methode of Newton to solve a second degree equation

$$df_dQinner(i) = 2 * K_inner_leg(i) * Q_inner(i) + 2 * K_outer_leg(i) * (Q(i) - Q_inner(i))$$

$$Q_inner_new(i) = Q_inner(i) - f_Qinner(i) / df_dQinner(i)$$

```
Worksheets("CasingLosses").Range("Z1") = "Hv_OuterLeg(m)"
Worksheets("CasingLosses").Range("Z" & i + 1) = Hv_OuterLeg(i)
Worksheets("CasingLosses").Range("AA1") = "Hv_InnerLeg(m)"
Worksheets("CasingLosses").Range("AA" & i + 1) = Hv_InnerLeg(i)
```

```
Worksheets("CasingLosses").Range("AB1") = "K_outer_leg"
Worksheets("CasingLosses").Range("AB" & i + 1) = K_outer_leg(i)
Worksheets("CasingLosses").Range("AC1") = "K_inner_leg"
Worksheets("CasingLosses").Range("AC" & i + 1) = K_inner_leg(i)
```

```
Worksheets("CasingLosses").Range("A1") = "Q(m3/s)"
Worksheets("CasingLosses").Range("A" & i + 1) = Q(i)
```

Next i

j = 1

Do

If Abs(f_Qinner(j)) > epsilon_Q Then

 Q_inner = Q_inner_new

 Flag = 0

Else

 j = j + 1

 Flag = 1

End If

Loop While Flag = 1 And j < NoPoints

Loop While Flag = 0

For i = 1 To NoPoints

```
Worksheets("CasingLosses").Range("AD1") = "Q_outer(m3/s)"
Worksheets("CasingLosses").Range("AD" & i + 1) = Q_outer(i)
Worksheets("CasingLosses").Range("AE1") = "Q_inner(m3/s)"
Worksheets("CasingLosses").Range("AE" & i + 1) = Q_inner(i)
Worksheets("CasingLosses").Range("AF1") = "f_Qinner"
Worksheets("CasingLosses").Range("AF" & i + 1) = f_Qinner(i)
```

Next i

' Plotting the volute losses according to the flow rate to power 2

Set Graph = Worksheets("CasingLosses").ChartObjects.Add(10, 220, 400, 250)

Graph.Chart.ChartType = xlXYScatter

Graph.Chart.SetSourceData Worksheets("CasingLosses").Range("A:A,F:F,J:J,N:N,Q:Q,Z:Z")

With Graph.Chart

 .HasTitle = True

 .ChartTitle.Characters.Text = "Outer volute losses"

 .Axes(xlCategory, xlPrimary).HasTitle = True

 .Axes(xlCategory, xlPrimary).AxisTitle.Characters.Text = "Q[m^3/s]"

 .Axes(xlValue, xlPrimary).HasTitle = True

 .Axes(xlValue, xlPrimary).AxisTitle.Characters.Text = "Hv[m]"

End With

Set Graph = Worksheets("CasingLosses").ChartObjects.Add(420, 220, 400, 250)

Graph.Chart.ChartType = xlXYScatter

Graph.Chart.SetSourceData Worksheets("CasingLosses").Range("A:A,U:U,X:X,AA:AA")

With Graph.Chart

 .HasTitle = True

 .ChartTitle.Characters.Text = "Inner volute losses"

 .Axes(xlCategory, xlPrimary).HasTitle = True

 .Axes(xlCategory, xlPrimary).AxisTitle.Characters.Text = "Q[m^3/s]"

 .Axes(xlValue, xlPrimary).HasTitle = True

 .Axes(xlValue, xlPrimary).AxisTitle.Characters.Text = "Hv[m]"

End With

'Assesment of the losses in the runner

```

ReDim zFrictionBend(1 To NoPoints), zTotalBend(1 To NoPoints), kLocalBend(1 To NoPoints), kFrictionBend(1 To NoPoints)
ReDim kTotalBend(1 To NoPoints)
ReDim RunnerHeadLosses(1 To NoPoints), BendLosses(1 To NoPoints), FrictionLosses(1 To NoPoints)
ReDim cLaz(1 To NoPoints), Re_La(1 To NoPoints), Lambda(1 To NoPoints)

```

```

'Friction losses in the runner

```

```

A1q = Worksheets("RunnerGeometry").Range("K8").Value
A2q = Worksheets("RunnerGeometry").Range("N8").Value
Dh1 = Worksheets("RunnerGeometry").Range("K11").Value
Dh2 = Worksheets("RunnerGeometry").Range("N11").Value

```

```

Dhx = Sqr((A1q + A2q) / 2)
Dheq = (Dh1 + Dh2 + 2 * Dhx) / 4
DeltaRelative = RoughnessRunner / Dheq

```

```

For j = 1 To NoPoints

```

```

    cLaz(j) = 0.5 * QLaz(j) * ((A1q + A2q) / (A1q * A2q))
    Re_La(j) = Reynolds(cLaz(j), Dheq, Viscosity)
    Lambda(j) = TubeFrictionCoefficient(Re_La(j), DeltaRelative)

```

```

    Worksheets("RunnerLosses").Range("A1") = "Q(m3/s)"
    Worksheets("RunnerLosses").Range("A" & j + 1) = Q(j)
    Worksheets("RunnerLosses").Range("B1") = "QLaz(m3/s)"
    Worksheets("RunnerLosses").Range("B" & j + 1) = QLaz(j)
    Worksheets("RunnerLosses").Range("C1") = "Re (-)"
    Worksheets("RunnerLosses").Range("C" & j + 1) = Re_La(j)
    Worksheets("RunnerLosses").Range("D1") = "Lambda(-)"
    Worksheets("RunnerLosses").Range("D" & j + 1) = Lambda(j)

```

```

Next j

```

```

'Assesment of the bending losses in the runner

```

```

Rk = Worksheets("RunnerGeometry").Range("B24").Value
Delta° = Worksheets("RunnerGeometry").Range("B25").Value

```

```

For i = 1 To NoPoints

```

```

    zLocalBend = BendLocal(Delta°, Rk, Dheq)
    zFrictionBend(i) = BendFriction(Lambda(i), Rk, Dheq, Delta°)
    zTotalBend(i) = zLocalBend + zFrictionBend(i)

```

```

    kLocalBend(i) = zLocalBend / ((Pi * Dheq ^ 2 / 4) ^ 2)
    kFrictionBend(i) = zFrictionBend(i) / ((Pi * Dheq ^ 2 / 4) ^ 2)
    kTotalBend(i) = zTotalBend(i) / ((Pi * Dheq ^ 2 / 4) ^ 2)

```

```

    Worksheets("RunnerLosses").Range("E1") = "kLocalBend"
    Worksheets("RunnerLosses").Range("E" & i + 1) = kLocalBend(i)
    Worksheets("RunnerLosses").Range("G1") = "kFrictionBend"
    Worksheets("RunnerLosses").Range("G" & i + 1) = kFrictionBend(i)

```

```

    BendLosses(i) = 0.5 * kLocalBend(i) * (QLaz(i) ^ 2) / g
    FrictionLosses(i) = 0.5 * kFrictionBend(i) * (QLaz(i) ^ 2) / g
    RunnerHeadLosses(i) = 0.5 * kTotalBend(i) * (QLaz(i) ^ 2) / g

```

```

    Worksheets("RunnerLosses").Range("F1") = "BendLosses(m)"
    Worksheets("RunnerLosses").Range("F" & i + 1) = BendLosses(i)
    Worksheets("RunnerLosses").Range("H1") = "FrictionLosses(m)"
    Worksheets("RunnerLosses").Range("H" & i + 1) = FrictionLosses(i)
    Worksheets("RunnerLosses").Range("I1") = "TotalLosses(m)"
    Worksheets("RunnerLosses").Range("I" & i + 1) = RunnerHeadLosses(i)

```

```

Next i

```

```

' Plotting the runner losses according to the flow rate to power 2

```

```

Set Graph = Worksheets("RunnerLosses").ChartObjects.Add(600, 120, 400, 250)
Graph.Chart.ChartType = xlXYScatter
Graph.Chart.SetSourceData Worksheets("RunnerLosses").Range("A:A,F:F,H:H,I:I")
With Graph.Chart
    .HasTitle = True
    .ChartTitle.Characters.Text = "Assesment of the hydraulic losses in the runner"
    .Axes(xlCategory, xlPrimary).HasTitle = True
    .Axes(xlCategory, xlPrimary).AxisTitle.Characters.Text = "Q[m^3/s]"
    .Axes(xlValue, xlPrimary).HasTitle = True
    .Axes(xlValue, xlPrimary).AxisTitle.Characters.Text = "H[m]"
End With

```

```

*****

```

```

'* Assesment of the sudden section changes

```

```
A1 = Worksheets("RunnerGeometry").Range("B9").Value
e1x = Worksheets("RunnerGeometry").Range("B17").Value
B1 = Worksheets("RunnerGeometry").Range("B10").Value
e2x = Worksheets("RunnerGeometry").Range("E17").Value
e2 = Worksheets("RunnerGeometry").Range("E18").Value
A2 = Worksheets("RunnerGeometry").Range("E9").Value
b2 = Worksheets("RunnerGeometry").Range("E10").Value
B3 = Worksheets("RunnerGeometry").Range("H7").Value
d2 = Worksheets("RunnerGeometry").Range("E6").Value
```

```
Ain2_1 = (A2 + e2x) * b2
Ain2_2 = ((Pi * d2 / zLa) - e2) * B3
Aout2 = ((Pi * d2 / zLa) - e2) * b2
```

```
zSuddenContr2_1 = SuddenContraction(Ain2_1, A2q) ' Sudden contraction at the inlet of the runner
zSuddenContr2_2 = SuddenContraction(Ain2_2, Aout2) ' Sudden contraction between the volute and the runner
```

```
Worksheets("SuddenLosses").Range("G2") = "zSuddenContr2_1"
Worksheets("SuddenLosses").Range("H2") = zSuddenContr2_1
Worksheets("SuddenLosses").Range("G3") = "zSuddenContr2_2"
Worksheets("SuddenLosses").Range("H3") = zSuddenContr2_2
```

```
kSuddenContr2_1 = zSuddenContr2_1 / (A2q ^ 2)
kSuddenContr2_2 = zSuddenContr2_2 / (Aout2 ^ 2)
```

```
Worksheets("SuddenLosses").Range("I2") = "kSuddenContr2_1"
Worksheets("SuddenLosses").Range("J2") = kSuddenContr2_1
Worksheets("SuddenLosses").Range("I3") = "kSuddenContr2_2"
Worksheets("SuddenLosses").Range("J3") = kSuddenContr2_2
```

```
Aout1 = (A1 + e1x) * B1
zSuddenExp1 = SuddenExpansion(A1q, Aout1) ' Sudden expansion at the outlet of the runner
kSuddenExp1 = zSuddenExp1 / (A1q ^ 2)
```

```
Worksheets("SuddenLosses").Range("G4") = "zSuddenExpan1"
Worksheets("SuddenLosses").Range("H4") = zSuddenExp1
Worksheets("SuddenLosses").Range("I4") = "kSuddenExp1"
Worksheets("SuddenLosses").Range("J4") = kSuddenExp1
```

```
ReDim SuddenContrLosses2_1(1 To NoPoints), SuddenContrLosses2_2(1 To NoPoints), SuddenExpaLosses1(1 To NoPoints)
ReDim TotalSuddenLosses(1 To NoPoints)
```

```
For j = 1 To NoPoints
```

```
    SuddenContrLosses2_1(j) = 0.5 * kSuddenContr2_1 * (QLaz(j) ^ 2) / g
    SuddenContrLosses2_2(j) = 0.5 * kSuddenContr2_2 * (QLaz(j) ^ 2) / g
    SuddenExpaLosses1(j) = 0.5 * kSuddenExp1 * (QLaz(j) ^ 2) / g
    TotalSuddenLosses(j) = SuddenContrLosses2_1(j) + SuddenContrLosses2_2(j) + SuddenExpaLosses1(j)
```

```
    Worksheets("SuddenLosses").Range("A1") = "Q(m³/s)"
    Worksheets("SuddenLosses").Range("A" & j + 1) = Q(j)
    Worksheets("SuddenLosses").Range("B1") = "QLaz(m³/s)"
    Worksheets("SuddenLosses").Range("B" & j + 1) = QLaz(j)
    Worksheets("SuddenLosses").Range("C1") = "ContrLosses2_1(m)"
    Worksheets("SuddenLosses").Range("C" & j + 1) = SuddenContrLosses2_1(j)
    Worksheets("SuddenLosses").Range("D1") = "ContrLosses2_2(m)"
    Worksheets("SuddenLosses").Range("D" & j + 1) = SuddenContrLosses2_2(j)
    Worksheets("SuddenLosses").Range("E1") = "ExpanLosses1(m)"
    Worksheets("SuddenLosses").Range("E" & j + 1) = SuddenExpaLosses1(j)
    Worksheets("SuddenLosses").Range("F1") = "TotalSuddenLoss(m)"
    Worksheets("SuddenLosses").Range("F" & j + 1) = TotalSuddenLosses(j)
```

```
Next j
```

```
' Plotting the sudden losses according to the flow rate to power 2
```

```
Set Graph = Worksheets("SuddenLosses").ChartObjects.Add(500, 120, 400, 250)
Graph.Chart.ChartType = xlXYScatter
Graph.Chart.SetSourceData Worksheets("SuddenLosses").Range("A:A,C:F")
With Graph.Chart
    .HasTitle = True
    .ChartTitle.Characters.Text = "Assesment of the sudden losses"
    .Axes(xlCategory, xlPrimary).HasTitle = True
    .Axes(xlCategory, xlPrimary).AxisTitle.Characters.Text = "Q[m³/s]"
    .Axes(xlValue, xlPrimary).HasTitle = True
    .Axes(xlValue, xlPrimary).AxisTitle.Characters.Text = "H[m]"
End With
```

```

*****
'Summary of results
*****
For i = 1 To NoPoints

    TotalLosses(i) = TotalVoluteLosses(i) + RunnerHeadLosses(i) + TotalSuddenLosses(i)
    HeadPredicted(i) = TotalLosses(i) + Hth(i)

    Worksheets("TotalLosses").Range("A1") = "Q(m3/s)"
    Worksheets("TotalLosses").Range("A" & i + 1) = Q(i)
    Worksheets("TotalLosses").Range("B1") = "Hth(m)"
    Worksheets("TotalLosses").Range("B" & i + 1) = Hth(i)
    Worksheets("TotalLosses").Range("C1") = "VoluteLosses(m)"
    Worksheets("TotalLosses").Range("C" & i + 1) = TotalVoluteLosses(i)
    Worksheets("TotalLosses").Range("D1") = "RunnerLosses(m)"
    Worksheets("TotalLosses").Range("D" & i + 1) = RunnerHeadLosses(i)
    Worksheets("TotalLosses").Range("E1") = "AbruptLosses(m)"
    Worksheets("TotalLosses").Range("E" & i + 1) = TotalSuddenLosses(i)
    Worksheets("TotalLosses").Range("F1") = "TotalLosses(m)"
    Worksheets("TotalLosses").Range("F" & i + 1) = TotalLosses(i)
    Worksheets("TotalLosses").Range("G1") = "HeadPredicted(m)"
    Worksheets("TotalLosses").Range("G" & i + 1) = HeadPredicted(i)
Next i

'Regression lineaire autour du BEP (Y=mo*X+Yo)

m = Application.WorksheetFunction.Slope(HeadPredicted, Q)
yo = Application.WorksheetFunction.Intercept(HeadPredicted, Q)

' Plotting the results

Set Graph = Worksheets("TotalLosses").ChartObjects.Add(500, 300, 400, 250)
Graph.Chart.ChartType = xlXYScatter
Graph.Chart.SetSourceData Worksheets("TotalLosses").Range("A:A,C:F")
With Graph.Chart
    .HasTitle = True
    .ChartTitle.Characters.Text = "Total Losses in turbine"
    .Axes(xlCategory, xlPrimary).HasTitle = True
    .Axes(xlCategory, xlPrimary).AxisTitle.Characters.Text = "Q[m^3/s]"
    .Axes(xlValue, xlPrimary).HasTitle = True
    .Axes(xlValue, xlPrimary).AxisTitle.Characters.Text = "H[m]"
End With

Set Graph = Worksheets("TotalLosses").ChartObjects.Add(500, 60, 400, 250)
Graph.Chart.ChartType = xlXYScatter
Graph.Chart.SetSourceData Worksheets("TotalLosses").Range("A:A,B:B,F:F,G:G")
With Graph.Chart
    .HasTitle = True
    .ChartTitle.Characters.Text = "Summary of turbine characteristics"
    .Axes(xlCategory, xlPrimary).HasTitle = True
    .Axes(xlCategory, xlPrimary).AxisTitle.Characters.Text = "Q[m^3/s]"
    .Axes(xlValue, xlPrimary).HasTitle = True
    .Axes(xlValue, xlPrimary).AxisTitle.Characters.Text = "H[m]"
End With

*****
'Prediction of the flow rate at BEP
*****
nq_p = Worksheets("GeneralData").Range("B23").Value
Qpump_BEP = Worksheets("GeneralData").Range("B24").Value
pump_efficiency = Worksheets("GeneralData").Range("B25").Value

If pump_efficiency >= 0.7 And pump_efficiency <= 0.8 Then

    Cqmin = -0.000005 * nq_p ^ 3 + 0.001 * nq_p ^ 2 - 0.0523 * nq_p + 2.075
    Cqmax = 0.000792 * nq_p ^ 2 - 0.0545 * nq_p + 2.2592

    RangeCq = Cqmax - Cqmin
    RangeEfficiency = 0.1
    Factor_ = (0.8 - pump_efficiency) / RangeEfficiency
    Cq_calcul = Cqmin + Factor_ * RangeCq

Else

    If pump_efficiency > 0.8 And pump_efficiency <= 0.86 Then

        Cqmin = -0.0000005 * nq_p ^ 3 + 0.000375 * nq_p ^ 2 - 0.0241 * nq_p + 1.6148
        Cqmax = -0.000005 * nq_p ^ 3 + 0.001 * nq_p ^ 2 - 0.0523 * nq_p + 2.075

```

```

RangeCq = Cqmax - Cqmin
RangeEfficiency = 0.06
Factor_ = (0.86 - pump_efficiency) / RangeEfficiency
Cq_calcul = Cqmin + Factor_ * RangeCq

End If

End If

Q_BEP_predict = Cq_calcul * Qpump_BEP * (1.055)

*****
'Determination of the BEP predicted
*****
H_predicted = m * Q_BEP_predict + yo

*****
'Determination of the efficiency at the BEP
*****

'Regression lineaire de Hth (Y=m1*X+Y1)

m1 = Application.WorksheetFunction.Slope(Hth, Q)
y1 = Application.WorksheetFunction.Intercept(Hth, Q)

Hth_BEP = m1 * Q_BEP_predict + y1
Hyd_Effic_BEP = Hth_BEP / H_predicted

Vol_efficiency_average = Application.WorksheetFunction.Average(VolumetricEffic)

Global_Effic_BEP = Hyd_Effic_BEP * MecanichEff * Vol_efficiency_average

*****
'Determination of Power Output at the BEP
*****

Power_predicted = (Rho * g * H_predicted * Q_BEP_predict * Global_Effic_BEP) / 1000

*****
'Comparison between turbine BEP predicted and turbine BEP promised by manufacturer
*****

H_promised = Worksheets("GeneralData").Range("B28").Value
Q_promised = Worksheets("GeneralData").Range("B29").Value
Eff_promised = Worksheets("GeneralData").Range("B30").Value
Pw_promised = (Rho * Q_promised * g * H_promised * Eff_promised) / 1000

Shift_H = (1 - (H_predicted / H_promised)) * 100
Shift_Q = (1 - (Q_BEP_predict / Q_promised)) * 100
Shift_Eff = (1 - (Global_Effic_BEP / Eff_promised)) * 100
Shift_Pw = (1 - (Power_predicted / Pw_promised)) * 100

'Print of comparisons

Worksheets("Resultats").Range("B1") = "Predicted"
Worksheets("Resultats").Range("C1") = "Manufacturer"
Worksheets("Resultats").Range("D1") = "Shift(%)"

Worksheets("Resultats").Range("A2") = "H(m)"
Worksheets("Resultats").Range("A3") = "Q(m)"
Worksheets("Resultats").Range("A4") = "Efficiency(-)"
Worksheets("Resultats").Range("A5") = "Power out (kW)"

Worksheets("Resultats").Range("B2") = H_predicted
Worksheets("Resultats").Range("B3") = Q_BEP_predict
Worksheets("Resultats").Range("B4") = Global_Effic_BEP
Worksheets("Resultats").Range("B5") = Power_predicted

Worksheets("Resultats").Range("C2") = H_promised
Worksheets("Resultats").Range("C3") = Q_promised
Worksheets("Resultats").Range("C4") = Eff_promised
Worksheets("Resultats").Range("C5") = Pw_promised

Worksheets("Resultats").Range("D2") = Shift_H
Worksheets("Resultats").Range("D3") = Shift_Q
Worksheets("Resultats").Range("D4") = Shift_Eff
Worksheets("Resultats").Range("D5") = Shift_Pw

End Sub

```

```

*****
'Functions used
*****

Function Reynolds(c, Dimension, Viscosity) As Double
Reynolds = c * Dimension / Viscosity
End Function

Function TubeFrictionCoefficient(Re, DeltaRelative) As Double
TubeFrictionCoefficient = 0.3086 / (Log10(0.135 * DeltaRelative + 6.5 / Re)) ^ 2
End Function

Function FlatPlateFrictionCoefficient(Re, DeltaRelative) As Double
FlatPlateFrictionCoefficient = 0.13 / (Log10(0.135 * DeltaRelative + 6.5 / Re)) ^ 2
End Function

Static Function Log10(X)
    Log10 = Log(X) / Log(10)
End Function

Function BendLocal(Delta, Rk, Dh) As Double
A1 = 1.6348 * (10 ^ -7) * (Delta ^ 3) - 8.1581 * (10 ^ -5) * (Delta ^ 2) + 1.714185 * (10 ^ -2) * Delta
If (Rk / Dh < 1) Then
    B1 = 0.21 * (Dh / Rk) ^ 2.5
Else
    B1 = 0.21 * (Dh / Rk) ^ 0.5
End If
C1 = 0.85
BendLocal = A1 * B1 * C1
End Function

Function BendFriction(Lambda, Rk, Dh, CurveAngle) As Double
BendFriction = 0.0175 * Lambda * (Rk / Dh) * CurveAngle
End Function

Function SuddenContraction(Ain, Aout) As Double
SuddenContraction = 0.5 * (1 - Aout / Ain)
End Function

Function SuddenExpansion(Ain, Aout) As Double
SuddenExpansion = (1 - Ain / Aout) ^ 2
End Function

Function LossCoefficientDiffuser(AR, Cpr) As Double
LossCoefficientDiffuser = 1 - Cpr - AR ^ -2
End Function

Function GradualExpansionLocal(Ain, Aout, alpha_rad) As Double
GradualExpansionLocal = k2 * (Tan(alpha_rad / 2)) ^ 1.25 * (1 - Ain / Aout) ^ 2
End Function

Function GradualExpansionFriction(Ain, Aout, Lambda, alpha_rad) As Double
GradualExpansionFriction = (Lambda / (8 * Sin(alpha_rad / 2))) * (1 - (Ain / Aout) ^ 2)
End Function

```